

# WP 5

## Control and Forecasting for Smart Energy Systems

**John Bagterp Jørgensen**

**Henrik Madsen, Jozsef Gaspar, Rune Grønberg Junker**

**CITIES Annual Meeting**

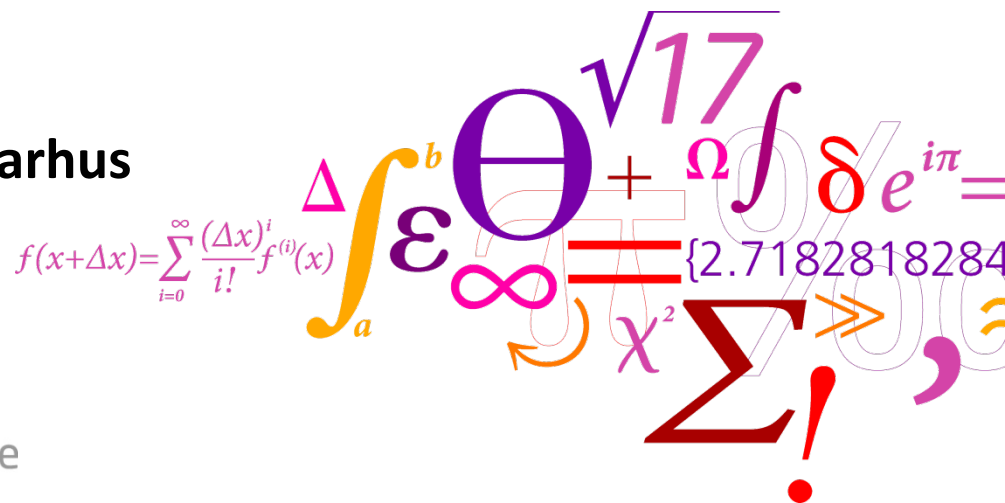
**May 30-31, 2017**

**Danish Technological Institute, Aarhus**

**DTU Compute**

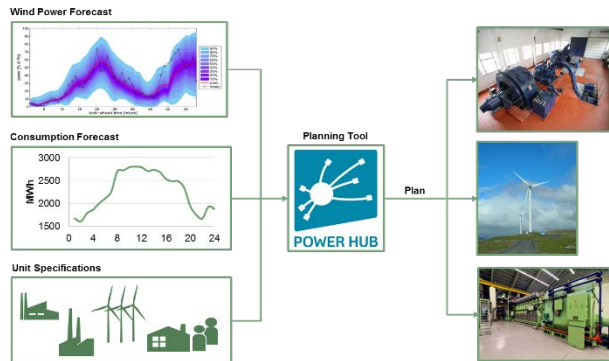
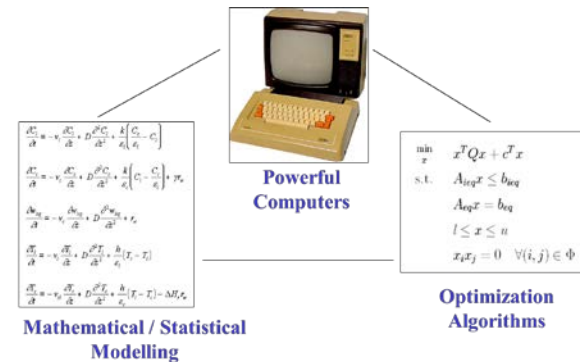
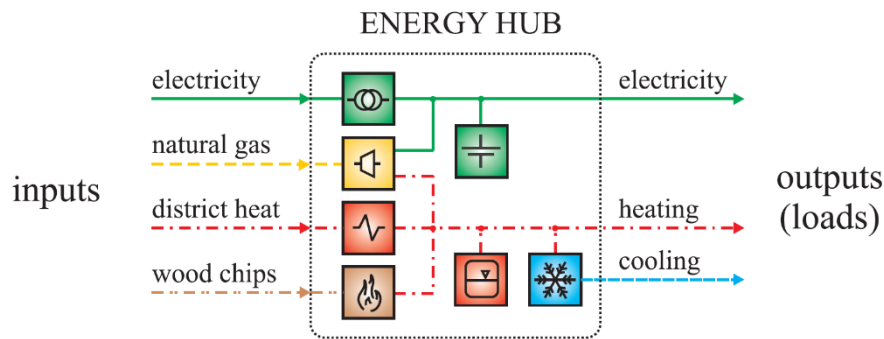
Institut for Matematik og Computer Science

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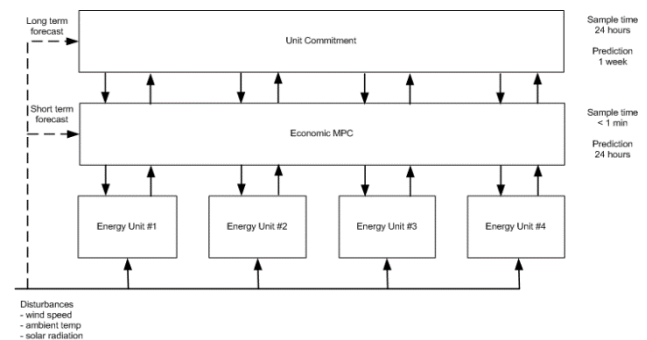


# Main Objectives

Develop and test optimization and forecast based predictive control systems for more efficient and flexible operation of integrated energy systems.



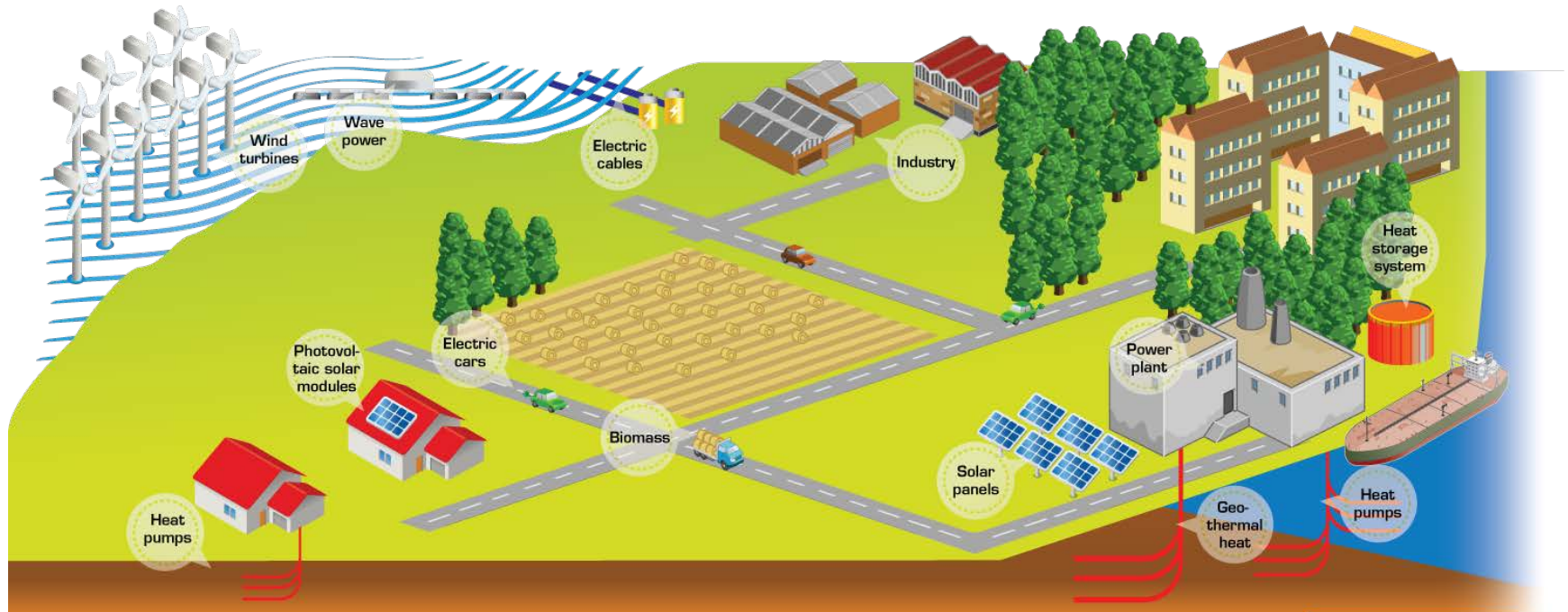
## Hierarchical Control Structure





# ENERGY SYSTEMS

# Smart Energy Systems



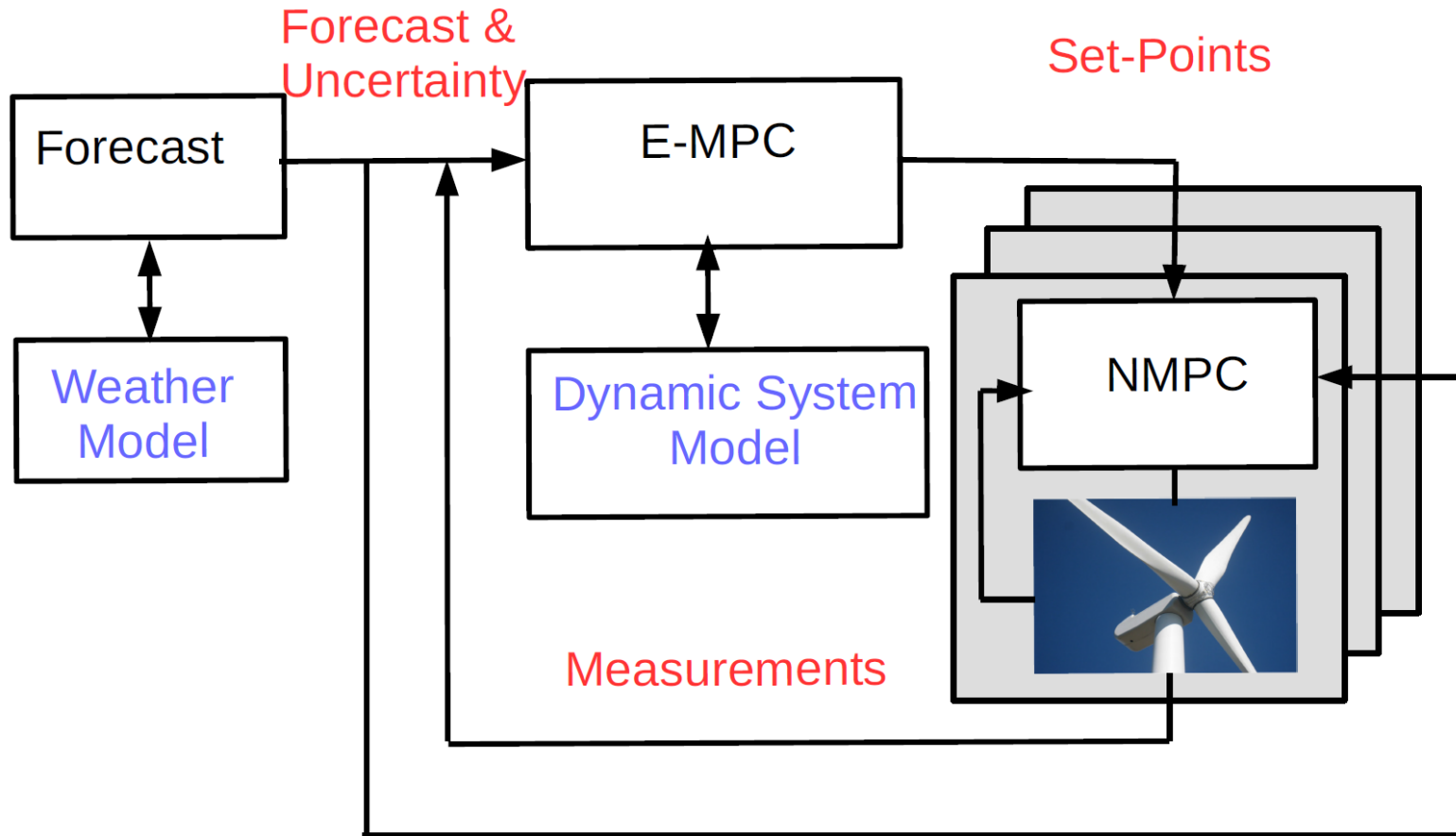
- **Thermal Storage**

- Heating of floors etc
- Heating of water accumulation tanks
- Refrigeration Systems

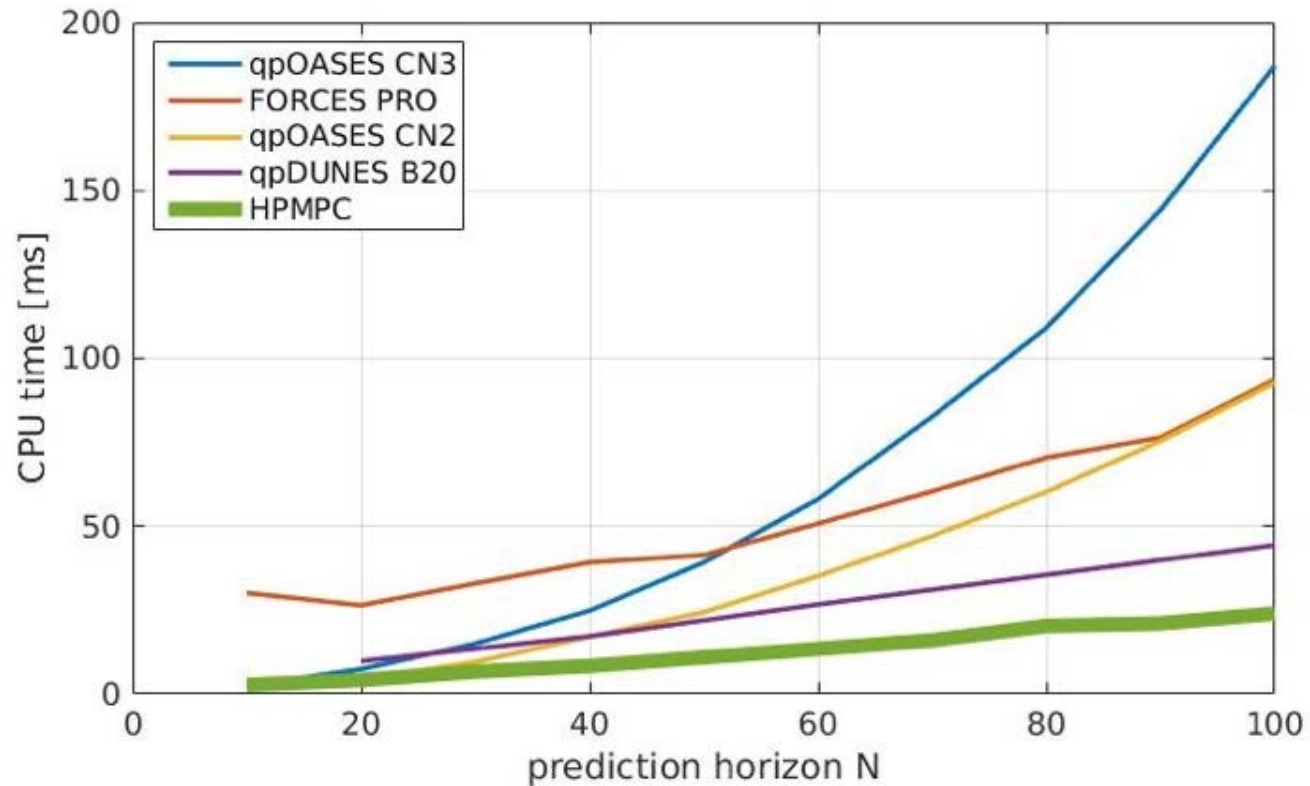
- **Power / Heat Producers**

- Wind Turbines
- Photovoltaic Solar Modules
- Solar Panels
- CHP Plants
- Fuel Cells

# Forecast Based Hierarchical MPC



# Computational Performance



# Drivers of MPC



**Powerful  
Computers**

$$\frac{\partial C_1}{\partial t} = -v_1 \frac{\partial C_1}{\partial z} + D \frac{\partial^2 C_1}{\partial z^2} + \frac{k}{\varepsilon_1} \left( \frac{C_c}{\varepsilon_1} - C_1 \right)$$

$$\frac{\partial C_c}{\partial t} = -v_c \frac{\partial C_c}{\partial z} + D \frac{\partial^2 C_c}{\partial z^2} + \frac{k}{\varepsilon_c} \left( C_1 - \frac{C_c}{\varepsilon_1} \right) + r_w$$

$$\frac{\partial w_{lig}}{\partial t} = -v_c \frac{\partial w_{lig}}{\partial z} + D \frac{\partial^2 w_{lig}}{\partial z^2} + r_w$$

$$\frac{\partial T_1}{\partial t} = -v_1 \frac{\partial T_1}{\partial z} + D \frac{\partial^2 T_1}{\partial z^2} + \frac{h}{\varepsilon_1} (T_c - T_1)$$

$$\frac{\partial T_c}{\partial t} = -v_{cl} \frac{\partial T_c}{\partial z} + D \frac{\partial^2 T_c}{\partial z^2} + \frac{h}{\varepsilon_c} (T_1 - T_c) - \Delta H_v r_w$$

**Mathematical / Statistical  
Modelling**

$$\begin{aligned} \min_x \quad & x^T Q x + c^T x \\ \text{s.t.} \quad & A_{ieq} x \leq b_{ieq} \\ & A_{eq} x = b_{eq} \\ & l \leq x \leq u \\ & x_i x_j = 0 \quad \forall (i, j) \in \Phi \end{aligned}$$

**Optimization  
Algorithms**

# Economic MPC

## Mathematical Optimization

The portfolio power generation problem can be stated as

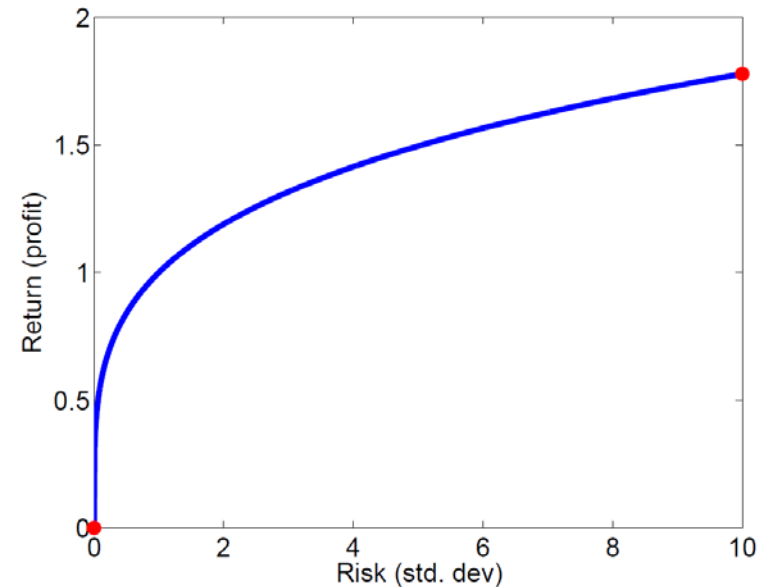
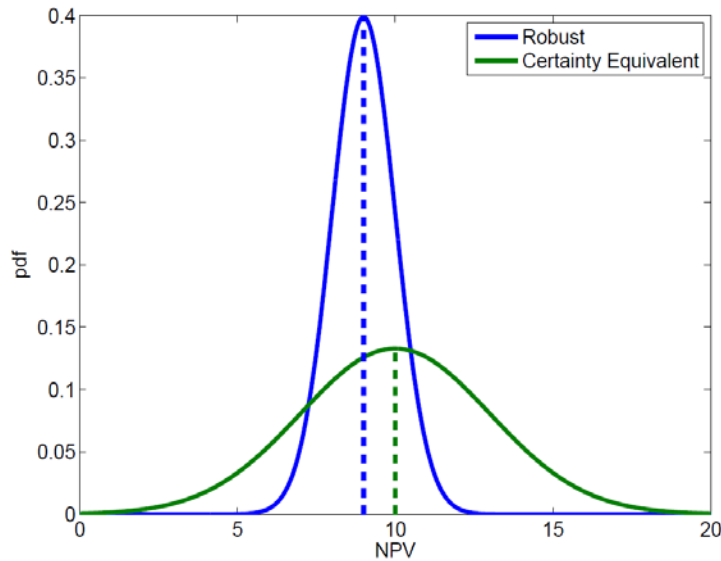
$$\begin{aligned}
 \min_{\{u_k\}_{k=0}^{N-1}} \quad & \phi = \sum_{k=0}^{N-1} c' u_k \\
 \text{s.t.} \quad & x_{k+1} = Ax_k + Bu_k + Ed_k \quad k = 0, 1, \dots, N-1 \\
 & y_k = Cx_k \quad k = 1, 2, \dots, N \\
 & u_{\min} \leq u_k \leq u_{\max} \quad k = 0, 1, \dots, N-1 \\
 & \Delta u_{\min} \leq \Delta u_k \leq \Delta u_{\max} \quad k = 0, 1, \dots, N-1 \\
 & y_k \geq r_k \quad k = 1, 2, \dots, N
 \end{aligned}$$

The parameters for this problem are

- Initial state,  $x_0$ , and previous decision,  $u_{-1}$
- Predicted loads on non-controllable generators (e.g. wind speed on wind turbines):  $\{d_k\}_{k=0}^{N-1}$
- Predicted power demand:  $\{r_k\}_{k=1}^N$

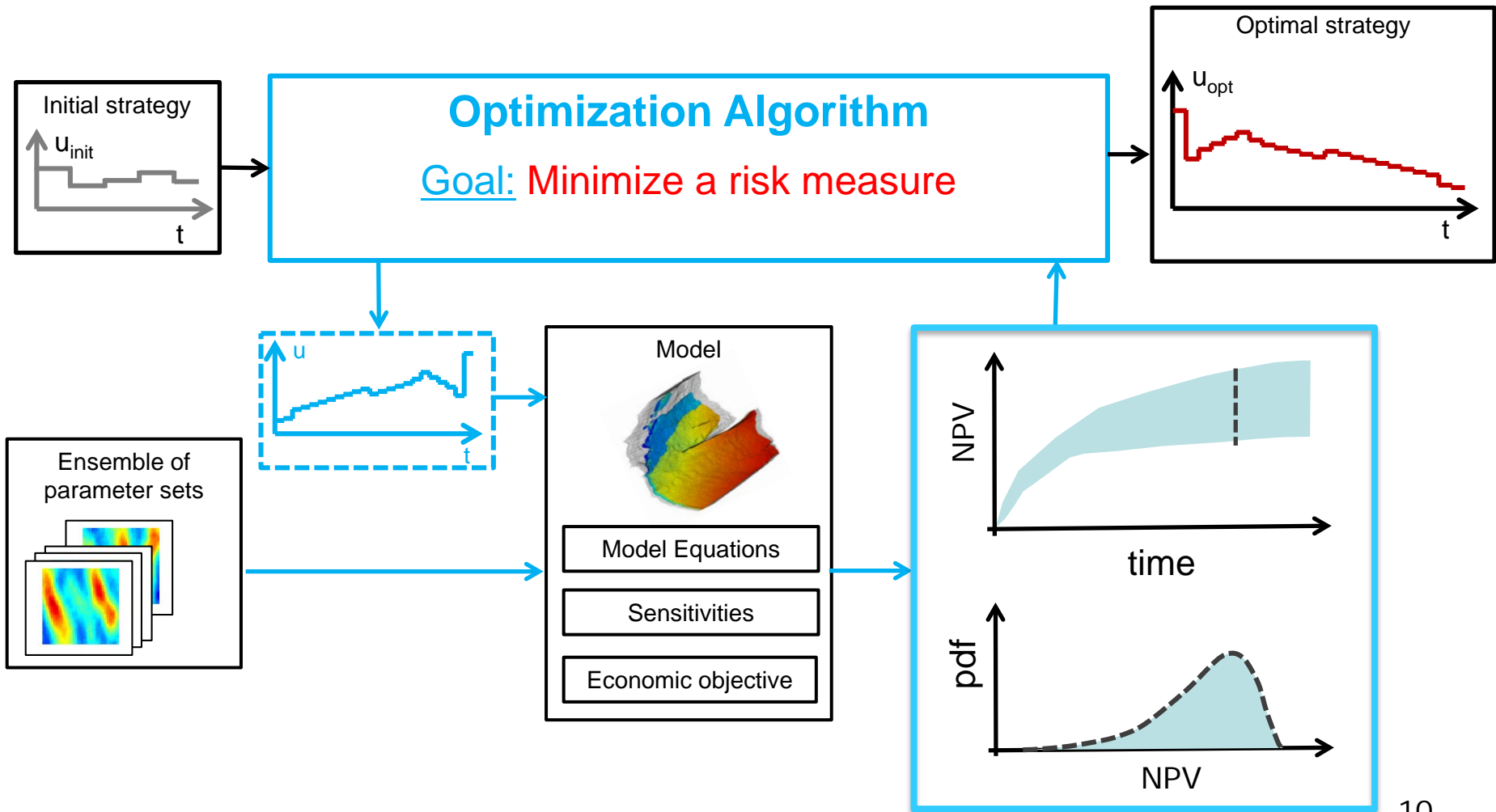


# Economic MPC for Uncertain Systems

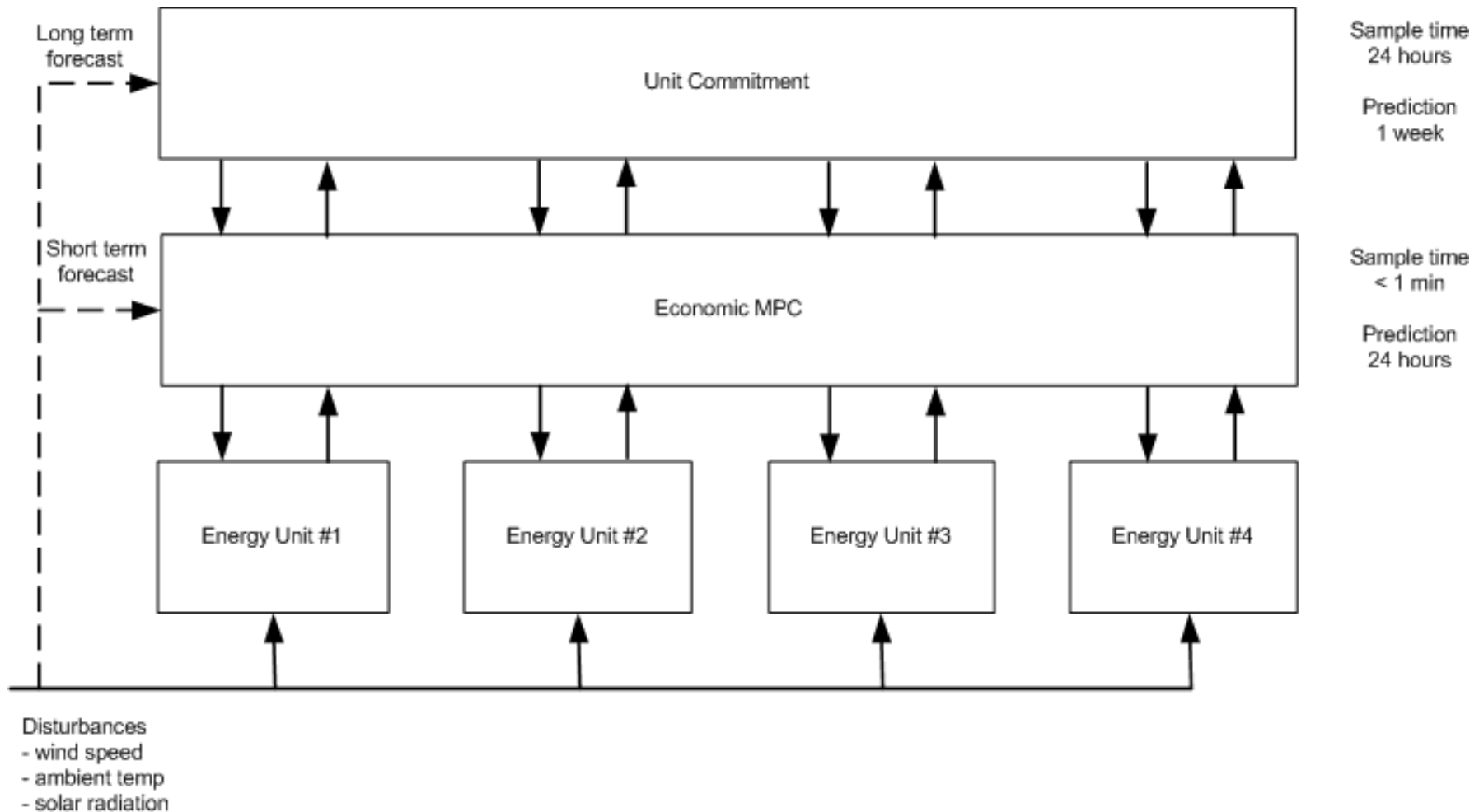


$$\max_{x \in \mathbb{R}^n} \psi(x) = \alpha \overbrace{E_{\theta} \{R(x, \theta)\}}^{\text{Mean profit}} - (1 - \alpha) \overbrace{V_{\theta} \{R(x, \theta)\}}^{\text{Profit variance}}$$

# Conditional Value at Risk (CVaR)

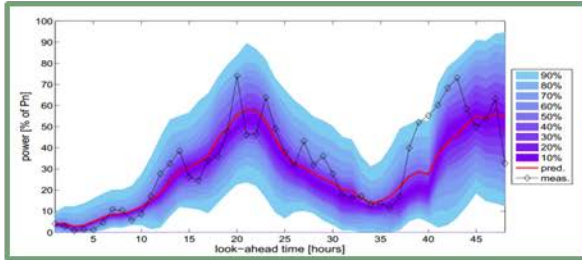


# Hierarchical Control Structure

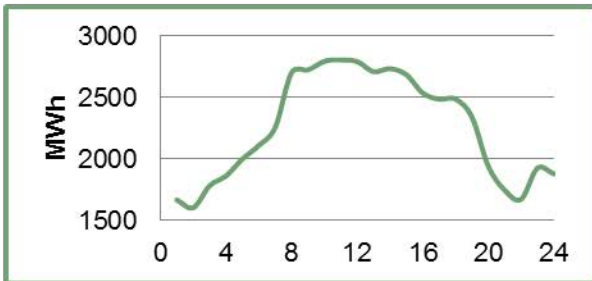


# Control of Smart Energy Systems = Economic MPC

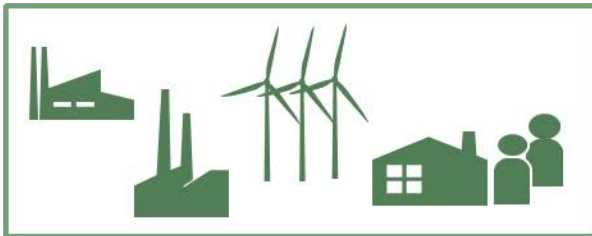
Wind Power Forecast



Consumption Forecast



Unit Specifications



Planning Tool



Plan



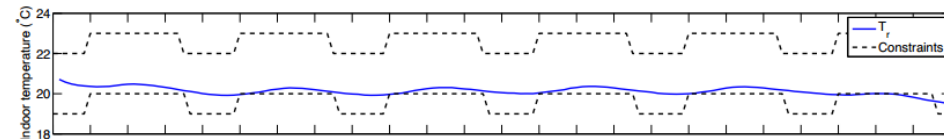
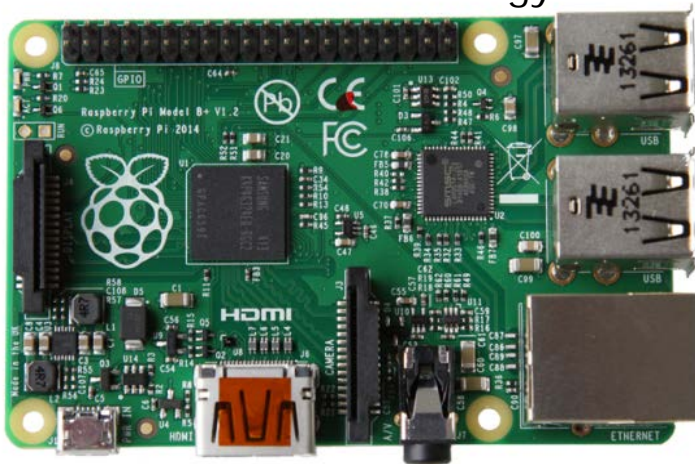


# ENERGY UNITS

# Control of Individual Energy Units

## Raspberry Pi

Embedded MPC Algorithms for control of individual energy units



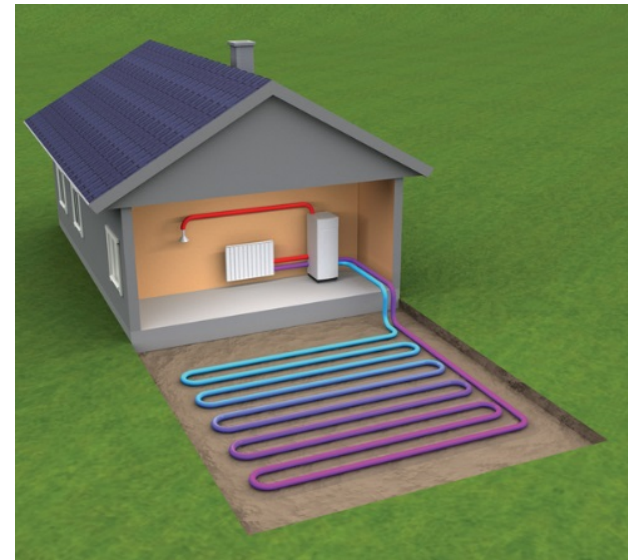
$$\min_{\{u_k, x_{k+1}\}_{k=0}^{N-1}} \phi = \sum_{k=0}^{N-1} l_k(x_k, u_k) + l_N(x_N) \quad (1a)$$

$$s.t. \quad x_{k+1} = A_k x_k + B_k u_k + b_k \quad k \in \mathcal{N} \quad (1b)$$

with  $\mathcal{N} = \{0, 1, \dots, N-1\}$  and stage costs defined by

$$l_k(x_k, u_k) = \frac{1}{2} \begin{bmatrix} x_k \\ u_k \end{bmatrix}' \begin{bmatrix} Q_k & M_k' \\ M_k & R_k \end{bmatrix} \begin{bmatrix} x_k \\ u_k \end{bmatrix} + \begin{bmatrix} q_k \\ s_k \end{bmatrix}' \begin{bmatrix} x_k \\ u_k \end{bmatrix} + \rho_k \quad (2a)$$

$$l_N(x_N) = \frac{1}{2} x_N' P_N x_N + p_N' x_N + \gamma_N \quad (2b)$$

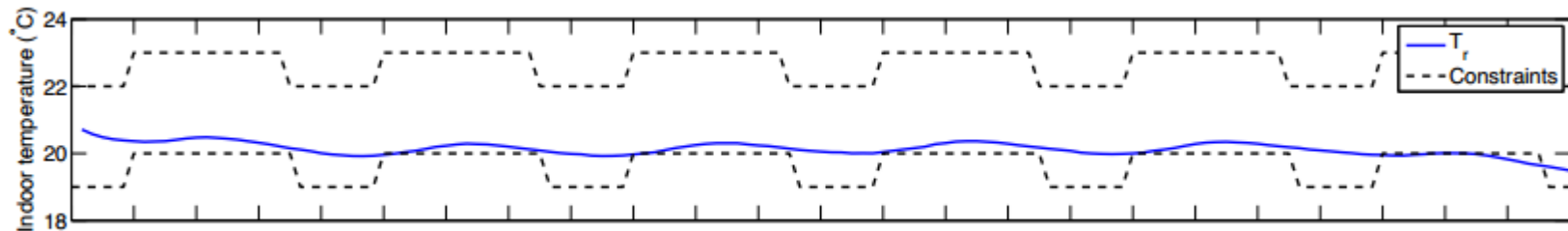


# Temperature Control

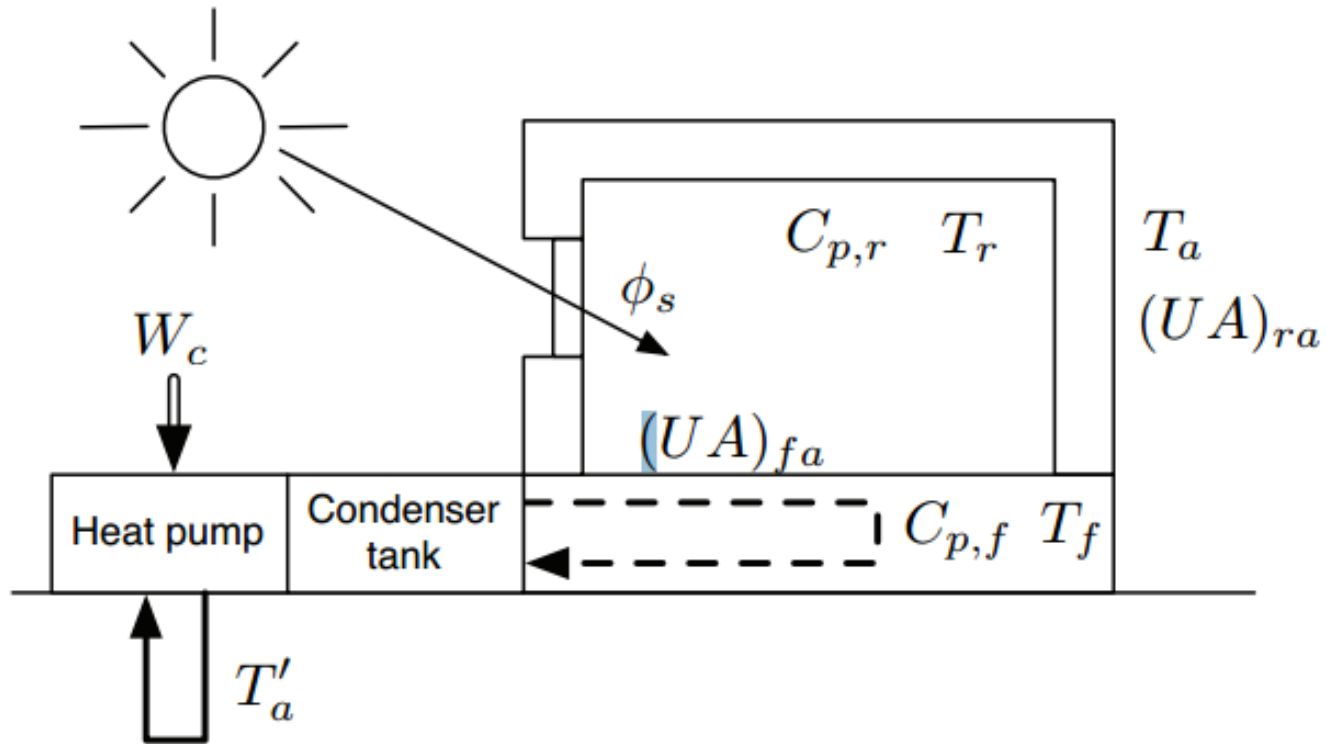
- Danfoss



- NEST (Google)



# Schematics of House with Heat Pump





# Model of a ground-source heated building

## Energy conservation

$$C_{pr}\dot{T}_r = Q_{fr} - Q_{ra} + (1 - p)\phi_{sol}$$

$$C_{pf}\dot{T}_f = Q_{wf} - Q_{fr} + p\phi_{sol}$$

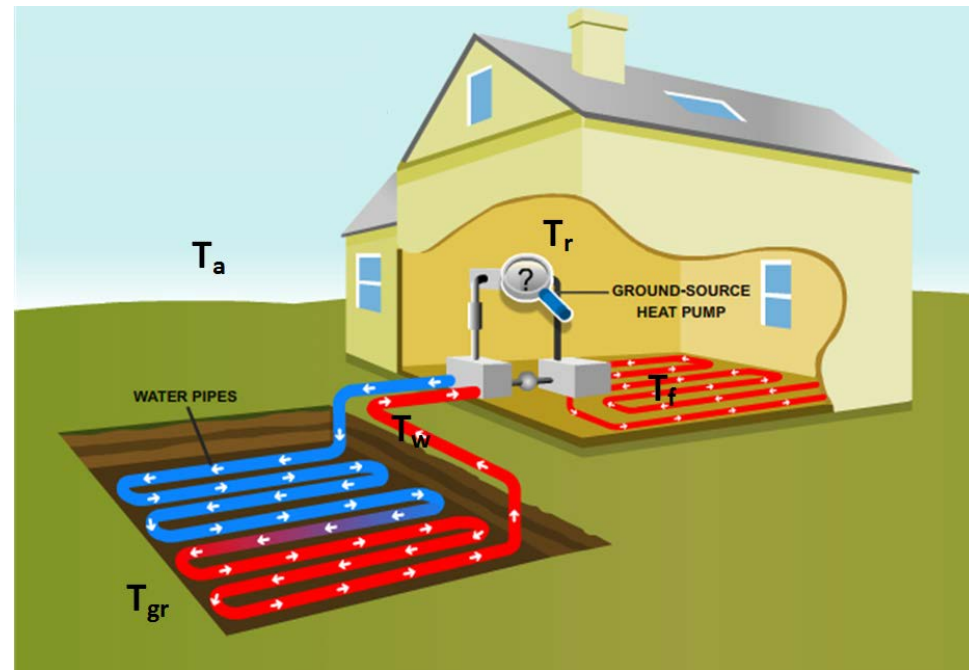
$$C_{pw}\dot{T}_w = Q_c - Q_{wf}$$

## Heat Transfer

$$Q_{fr} = UA_{fr}(T_f - T_r)$$

$$Q_{ra} = UA_{wf}(T_w - T_f)$$

$$Q_{fr} = UA_{ra}(T_r - T_a)$$



# Rigorous heat pump model

1 – 2: Isobar evaporation ( $\Delta P = 0$ )

2 – 3: Isentropic compression ( $\Delta S = 0$ )

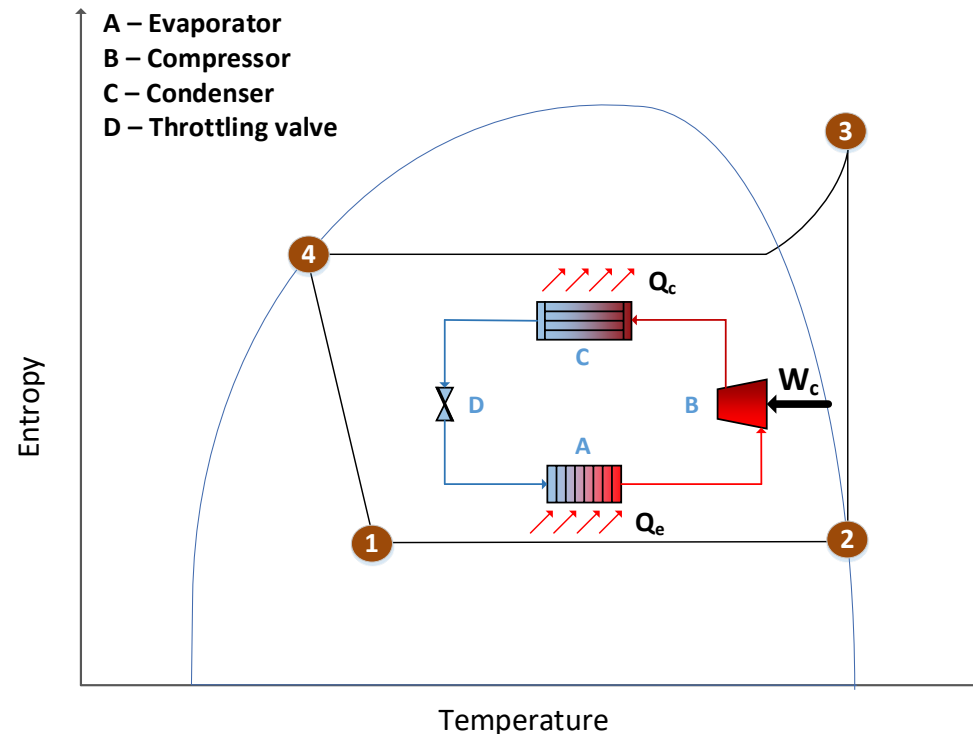
3 – 4: Isobar condensation ( $\Delta P = 0$ )

4 – 1: Isenthalpic expansion ( $\Delta H = 0$ )

$$W_c = \frac{Q_c}{\eta COP(T_w, T_{gr})}$$

$$COP = \frac{h_3(T_3, P_4) - h_4(T_w + \Delta T, P_4)}{h_3(T_3, P_4) - h_2(T_{gr} + \Delta T, P_2)}$$

**COP is a nonlinear function of  $T_w$  and  $T_{gr}$**



**Realistic Thermodynamics needed**

[www.psetools.org](http://www.psetools.org)

# Rigorous heat pump model

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## Algorithm 1: COP of a heat pump

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### Require:

Ground temperature,  $T_{gr}$

Water tank temperature,  $T_w$

Heat exchanger temperature difference,  $\Delta T$

### Compute using ThermoLib:

Evaporator pressure,  $P_2 = p_{sat}(T_2)$ , where

$T_2 = T_{gr} - \Delta T$

Enthalpy out from evaporator,  $h_2 = h(T_2, P_2)$

Entropy out from evaporator,  $s_2 = s(T_2, P_2)$

Condenser pressure,  $P_4 = p_{sat}(T_4)$ , where

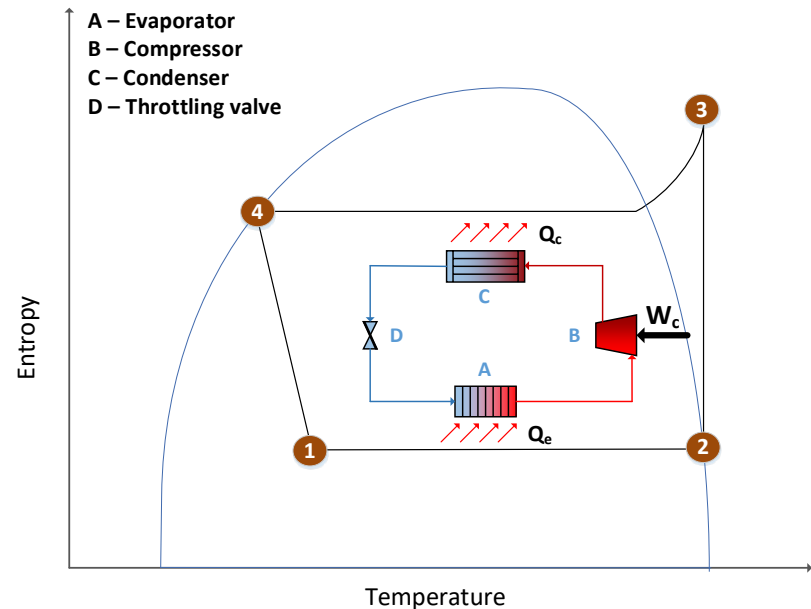
$T_4 = T_w + \Delta T$

Solve  $s_2 - s_3 = 0$  for  $T_3$ , where  $s_3 = s(T_3, P_4)$

Enthalpy out from compressor,  $h_3 = h(T_3, P_4)$

Enthalpy out from condenser,  $h_4 = h(T_4, P_4)$

$$COP = \frac{h_3(T_3, P_4) - h_4(T_w + \Delta T, P_4)}{h_3(T_3, P_4) - h_2(T_{gr} + \Delta T, P_2)}$$



**COP is a nonlinear function of  $T_w$  and  $T_{gr}$**

# Economic MPC

$$\begin{aligned} \min_{\hat{u}} \quad & \phi = \int_{t_0}^{t_f} (C(\hat{x}(t), \hat{u}(t), \hat{d}(t)) + V(\hat{y}(t))) dt, \\ \text{s.t.} \quad & \hat{x}(t_0) = \bar{x}_{k|k}, \quad k \geq 0 \\ & \dot{\hat{x}}(t) = A\hat{x}(t) + B\hat{u}(t) + E\hat{d}(t), \quad t \in [t_0, t_f] \\ & \hat{y}(t) = C\hat{x}(t), \quad t \in [t_0, t_f] \\ & u_{min}(t) \leq \hat{u}(t) \leq u_{max}(t), \quad t \in [t_0, t_f] \\ & \Delta u_{min}(t) \leq \Delta \hat{u}(t) \leq \Delta u_{max}(t), \quad t \in [t_0, t_f] \\ & y_{min}(t) - v(t) \leq \hat{y}(t), \quad t \in [t_0, t_f] \\ & y_{max}(t) + v(t) \geq \hat{y}(t), \quad t \in [t_0, t_f] \\ & v(t) \geq 0, \quad t \in [t_0, t_f] \end{aligned}$$

$$\hat{x} = [T_r \quad T_f \quad T_w]^T \quad \hat{u} = Q_c$$

$$\hat{y} = T_r$$

$$\hat{d} = [T_a \quad \phi_{sol}]^T$$

Energy cost function

Initial estimate from a Kalman filter

Linear house model

Bound constraints

Rate of change constraints

Soft thermal comfort constraints

# Economic MPC

**Special nonlinear  
economic MPC  
(NMPC)**

**Linear economic MPC  
(LMPC)**

**Linear economic MPC  
constant COP  
(LMPC w./ COP = 4.5)**

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Energy cost function:  $C(\hat{x}, \hat{u}, \hat{d}) = p_{el}(t)W_c(t)$

$$W_c = \frac{Q_c}{\eta COP(T_w, T_{gr})}$$

COP is calculated using estimates of  $T_w$  and forecasts of  $T_{gr}$

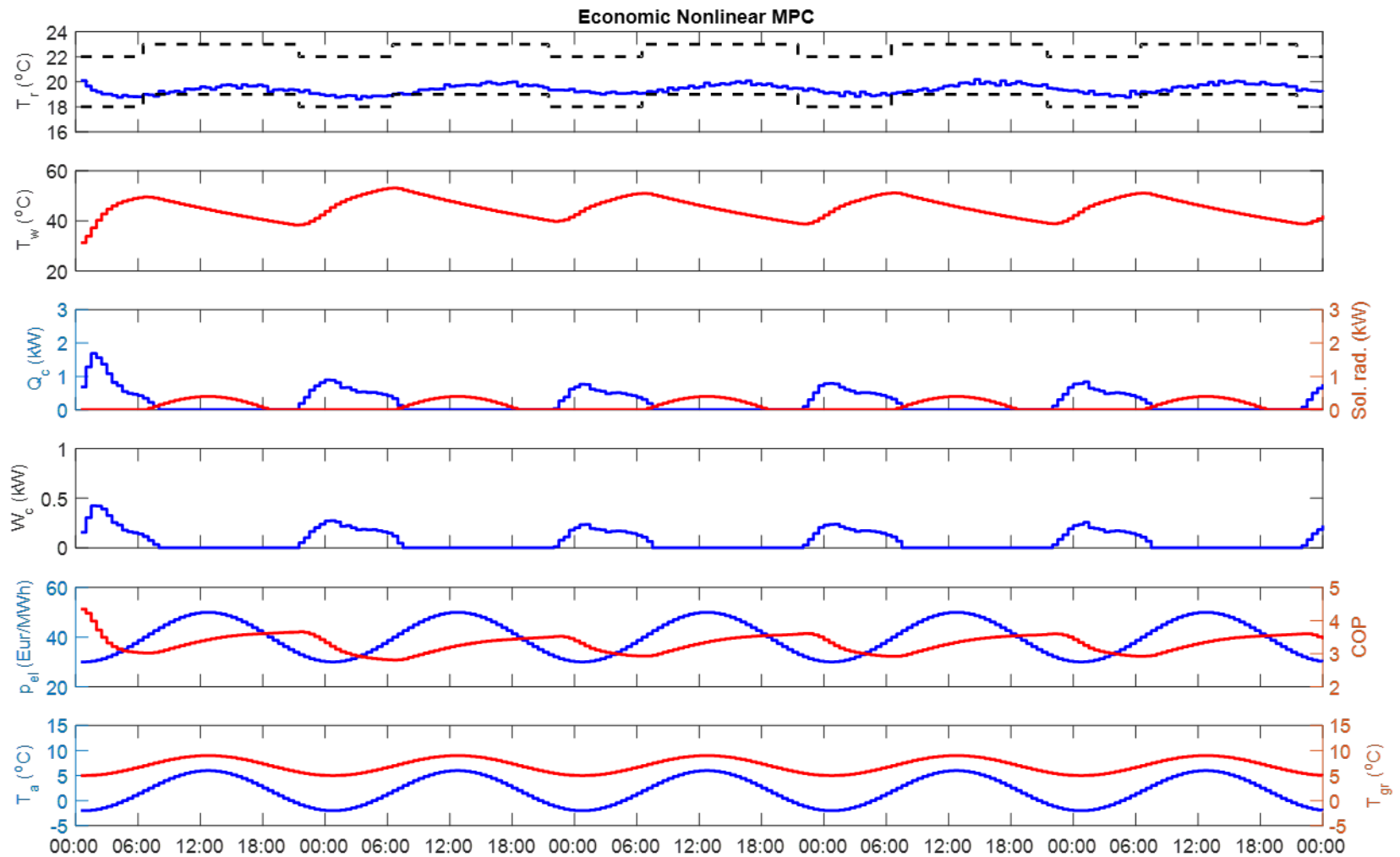
$$W_c = \frac{Q_c}{\eta COP}$$

COP is recalculated at each iteration step

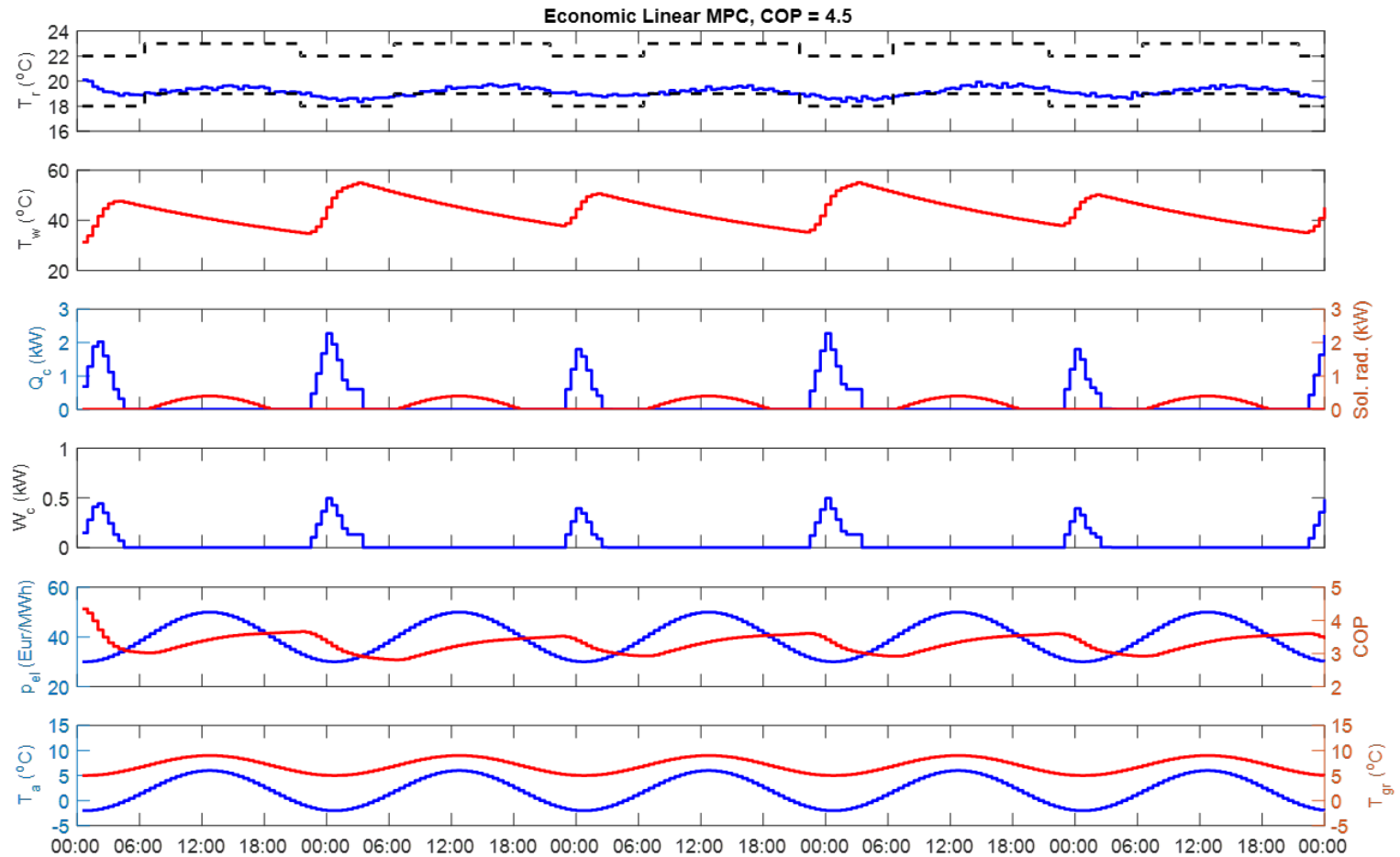
$$W_c = \frac{Q_c}{\eta COP}$$

COP is constant (COP = 4.5)

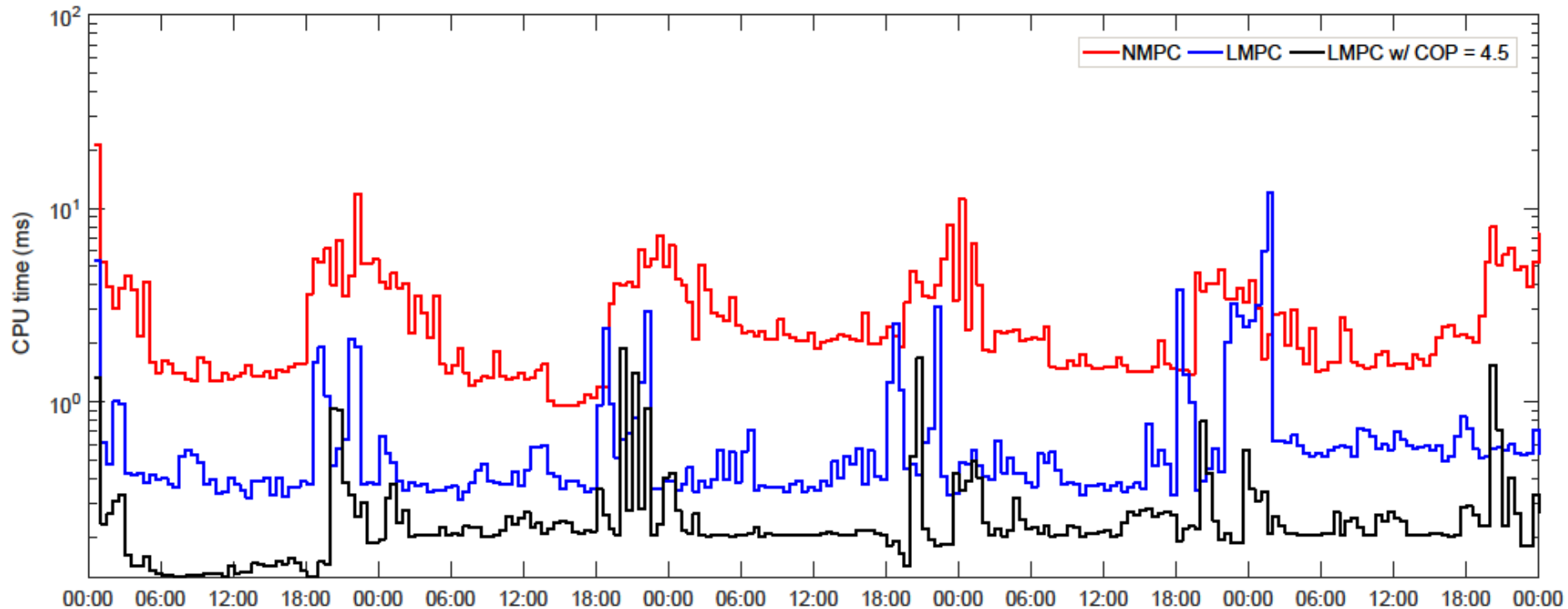
# Economic Nonlinear MPC



# Economic Linear MPC – Constant COP



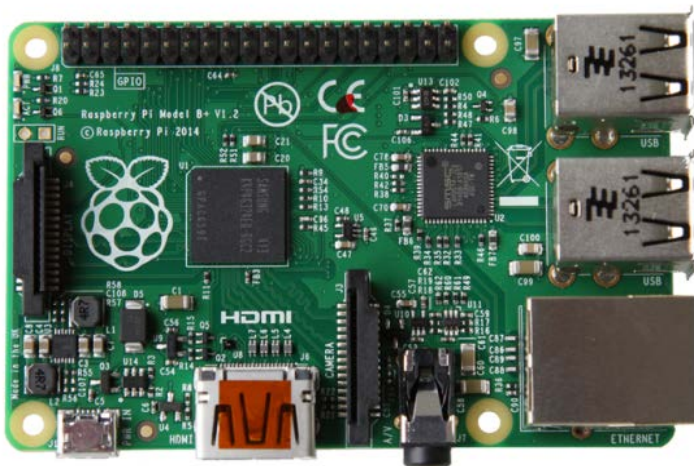
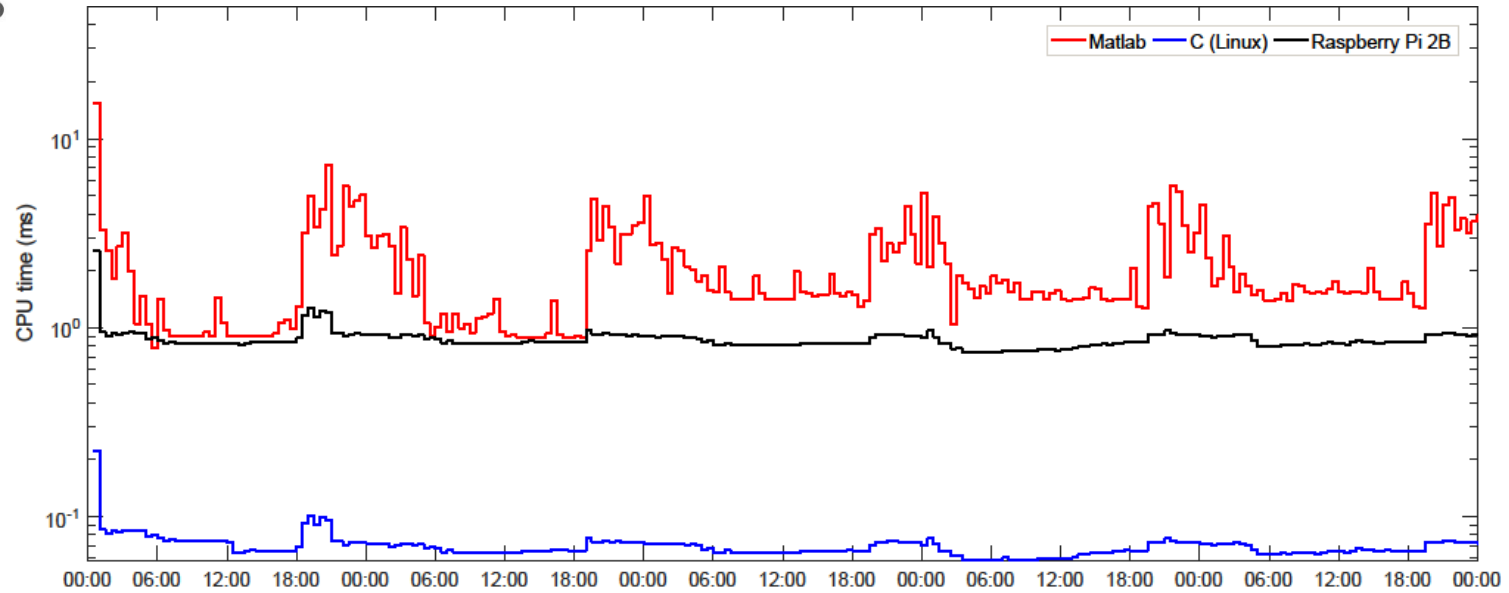
# Computational performance: NMPC vs LMPC



NMPC and LMPC have comparable computation time



# Computational performance: Matlab vs Linux-C



Simulation platform	Cold start (ms)	Average warm start (ms)
Raspberry Pi 2B	2.5	0.86
Workstation (C)	0.22	0.069
Workstation (Matlab)	15.51	2.07

## Features

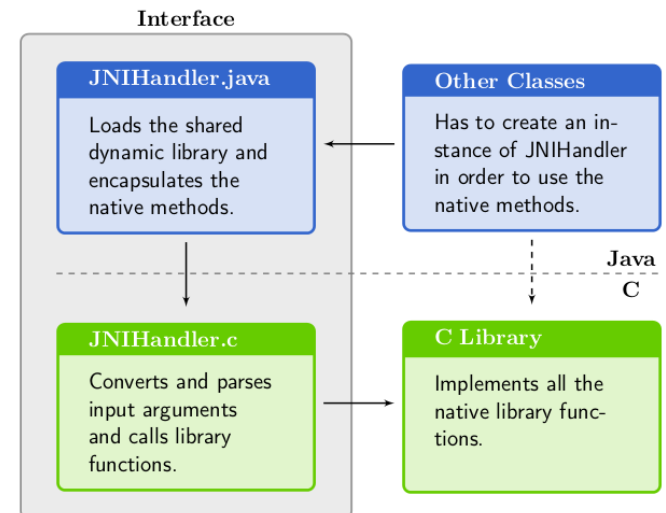
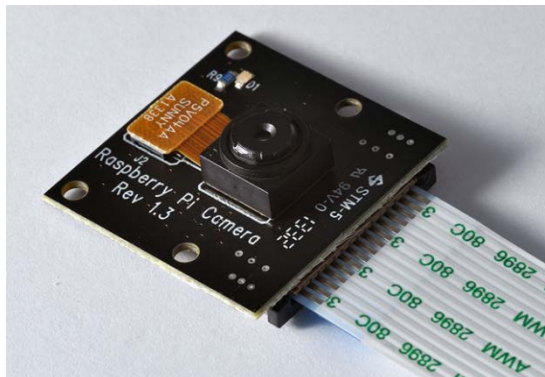
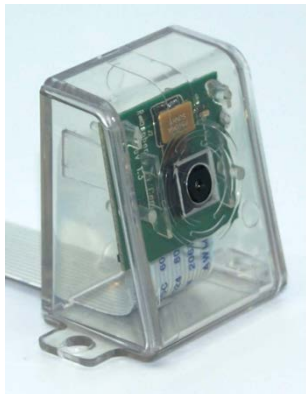
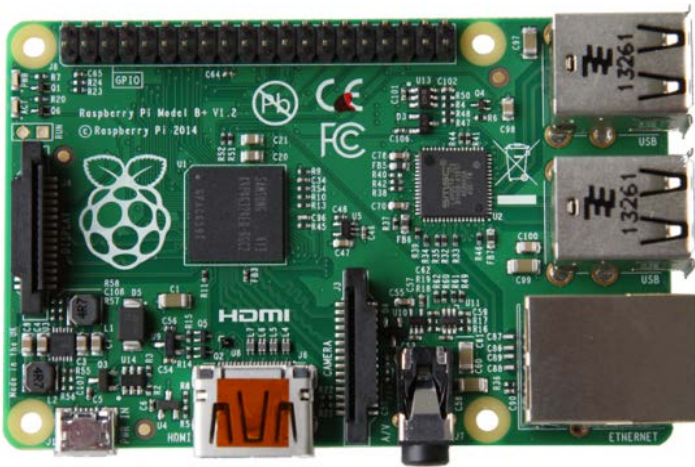
- Simplicity - easy to
  - Commission
  - Tune
  - Maintain
- Customizable and adaptable to
  - Process dynamics
  - Process modifications
  - Operational strategies
- Includes frontier technologies in
  - Mathematical Optimization
  - Process Control
  - Software Engineering
  - Mathematical/Statistical Modeling and Simulation



# Software Implementation

Raspberry Pi C/C++

Smart Phone C/Java/Matlab



# Thank You – Q & A



**John Bagterp Jørgensen**

Technical University of Denmark

E-mail: [jbjo@dtu.dk](mailto:jbjo@dtu.dk)

**DTU Compute**

Department of Applied Mathematics and Computer Science

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