

Energy Efficient Production of Pressurized Hydrogen - E2P2H2

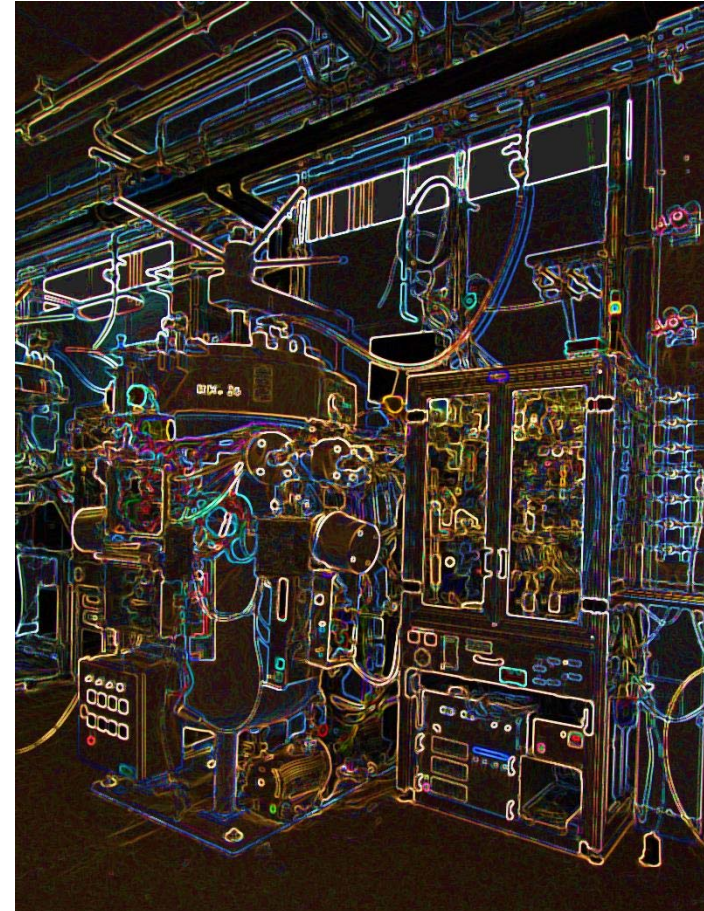
(EUDP project commenced by DTU Energi in collaboration with HTAS, 2014-2016)

Workshop, April 4th 2017

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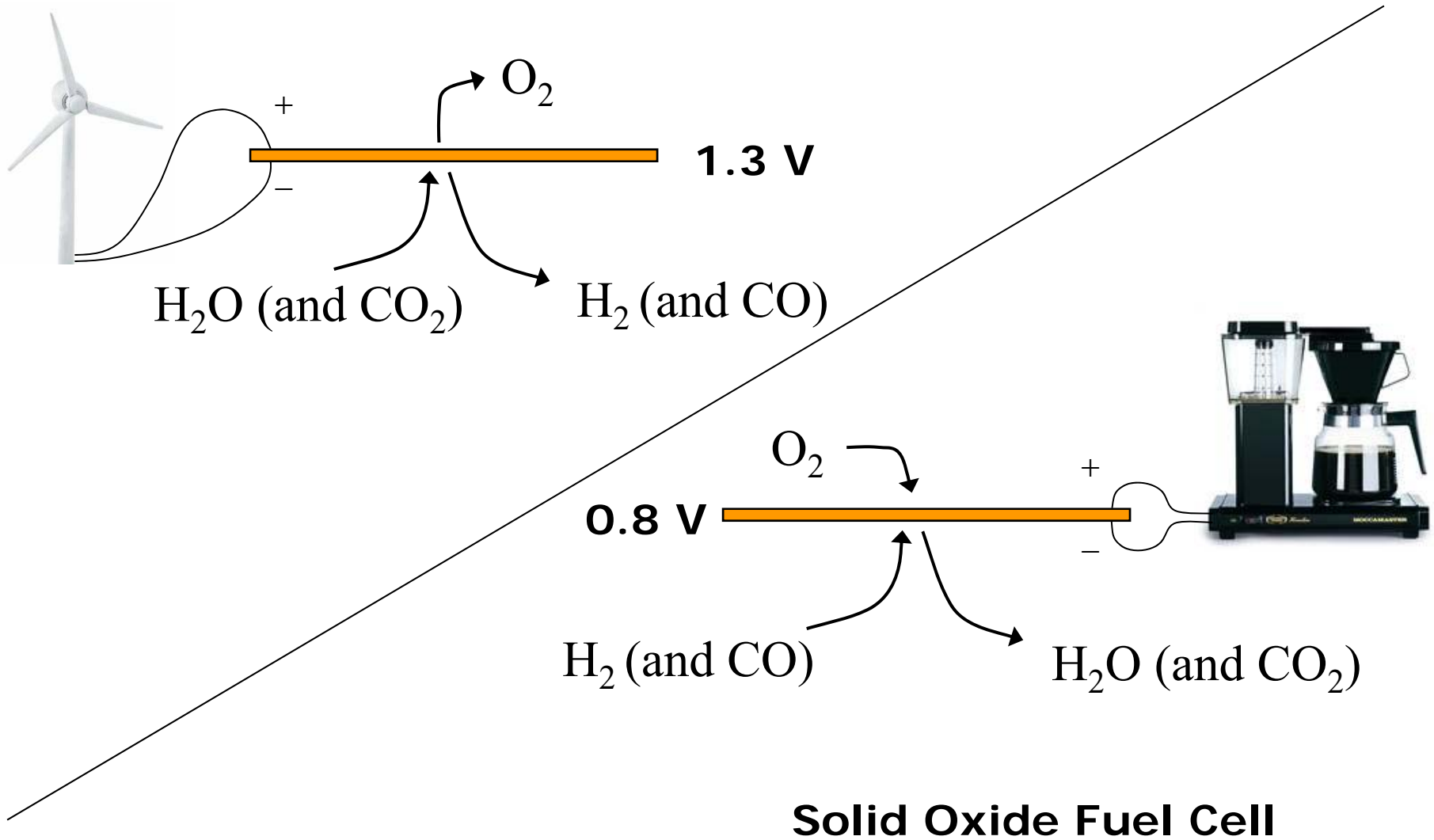


Cover on *FUEL CELLS 16* (2) 2016

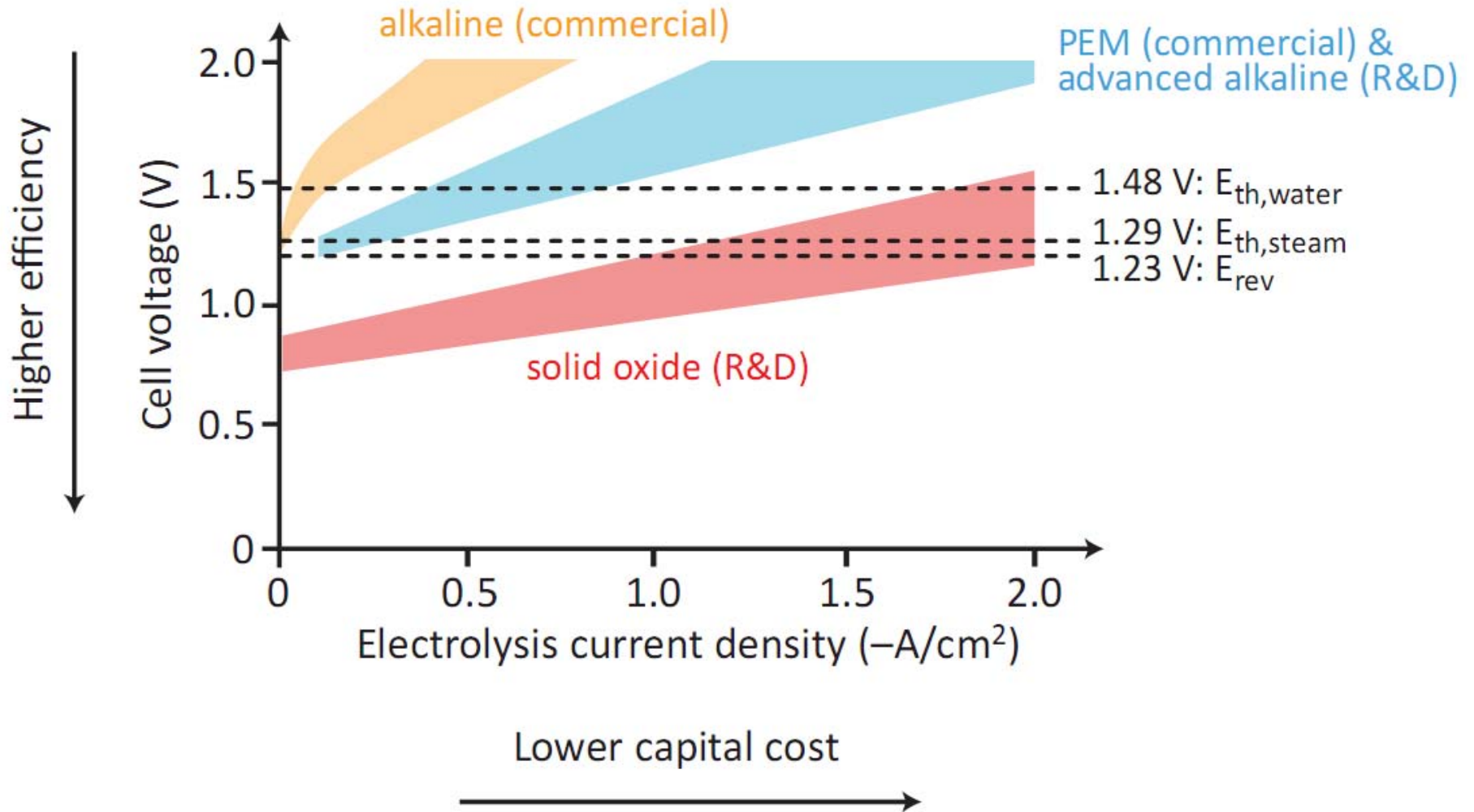
The Solid Oxide Cell



Solid Oxide Electrolysis Cell



Why Are Solid Oxide Electrolysers Interesting?



C. Graves, S.D. Ebbesen, M. Mogensen, K.S. Lackner, *Renewable and Sustainable Energy Reviews*. 15 (2011) 1–23

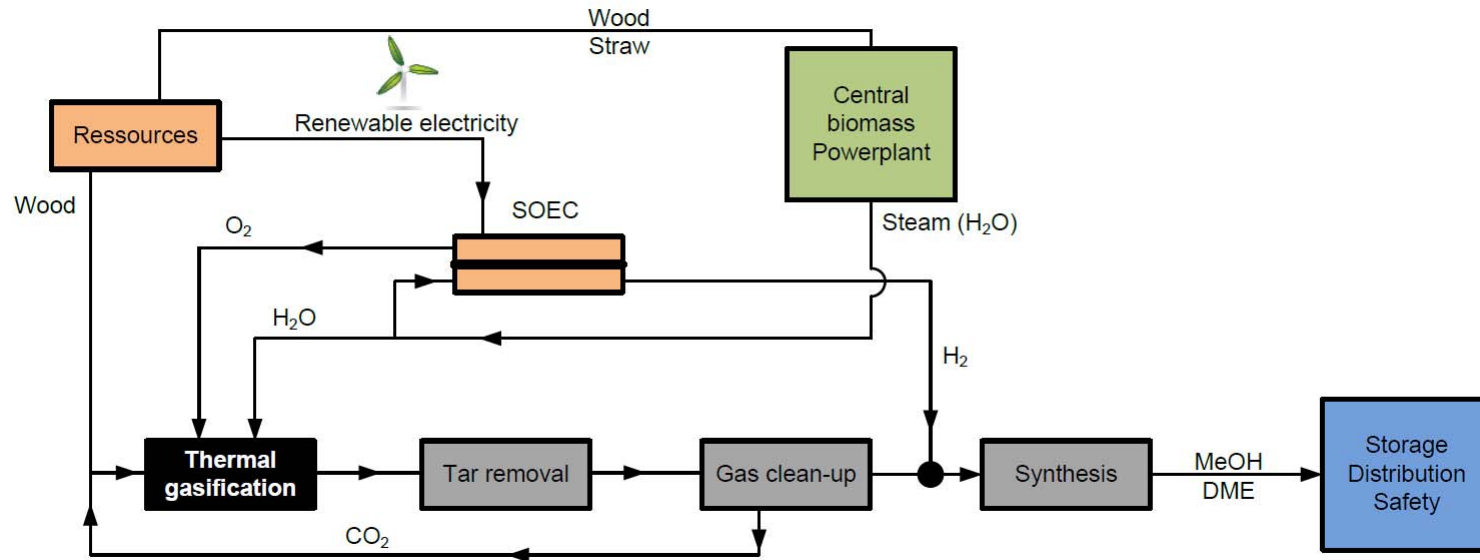
Synergy with utilization of biomass

- Biogas from biomass consist mostly of CO_2 (40%) and CH_4 (60%)
- If CO_2 in the biogas can react with H_2 we can generate app. 50% more CH_4



Photo: Mikael Kau/

SOEC Operating Strategy

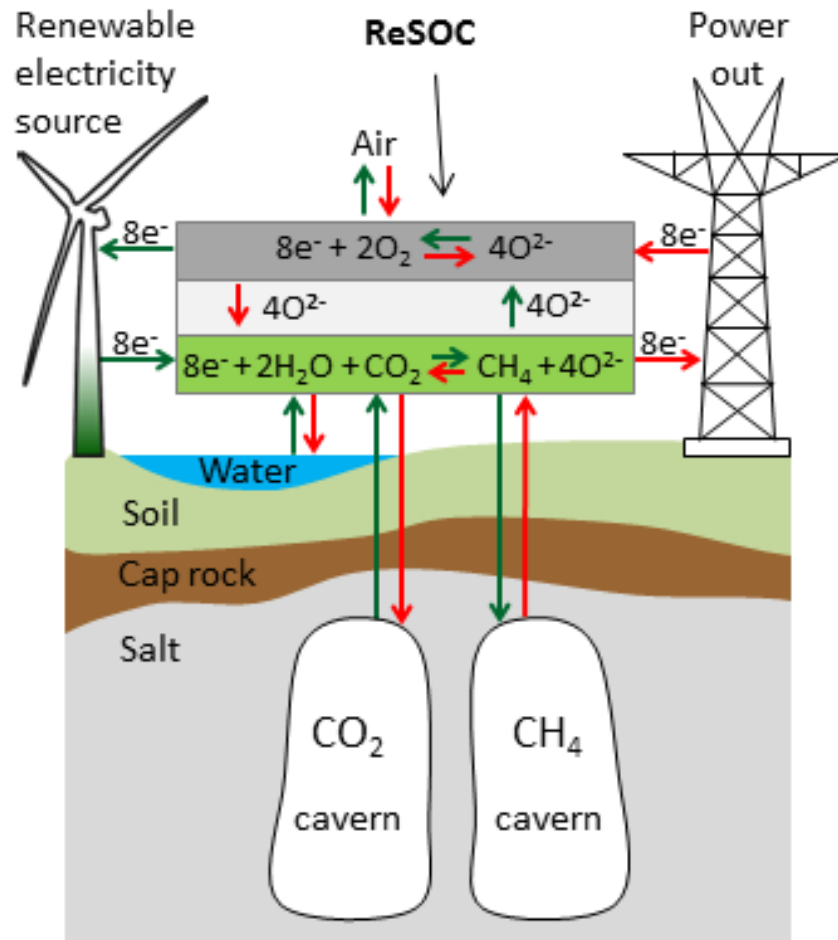


Two operating strategies

1. Always at optimal H-C ratio for the synthesis step
2. SOEC operates at 1/3 of nominal power at high electricity prices (generates enough O₂ for gasification)

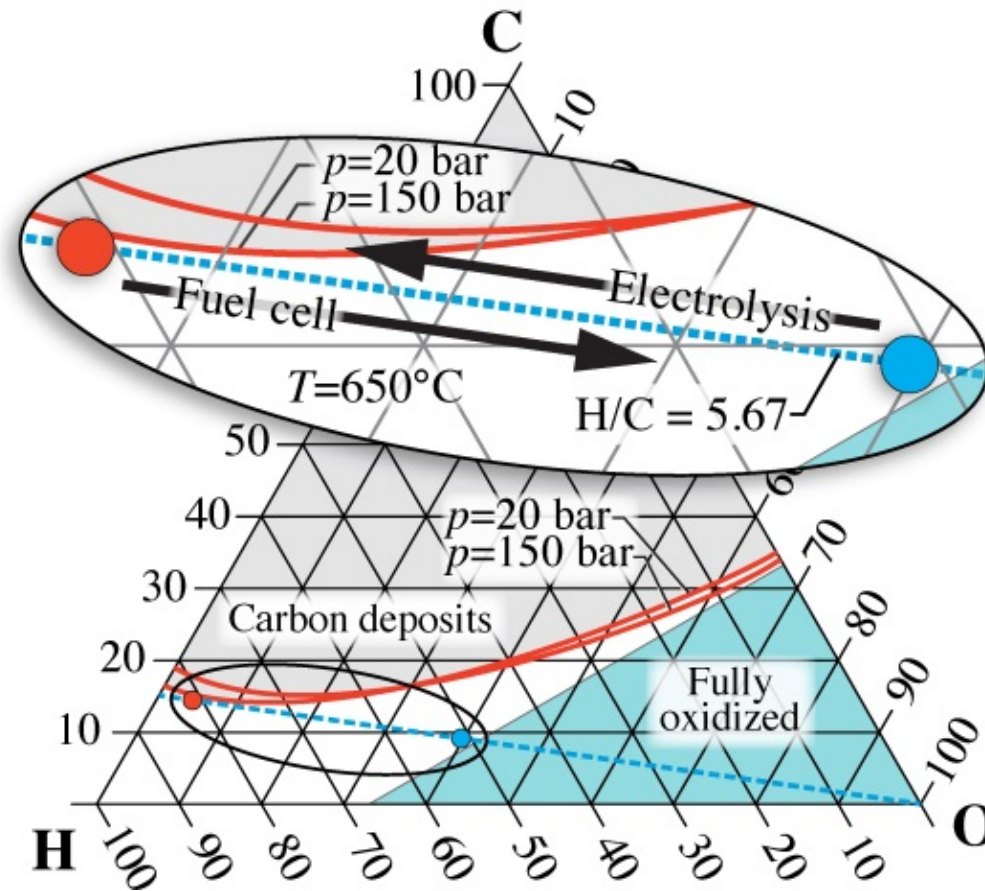
GreenSynFuels Report: <http://www.hydrogennet.dk/groennesynfuels/>

Pressurized SOCs for large-scale electricity storage



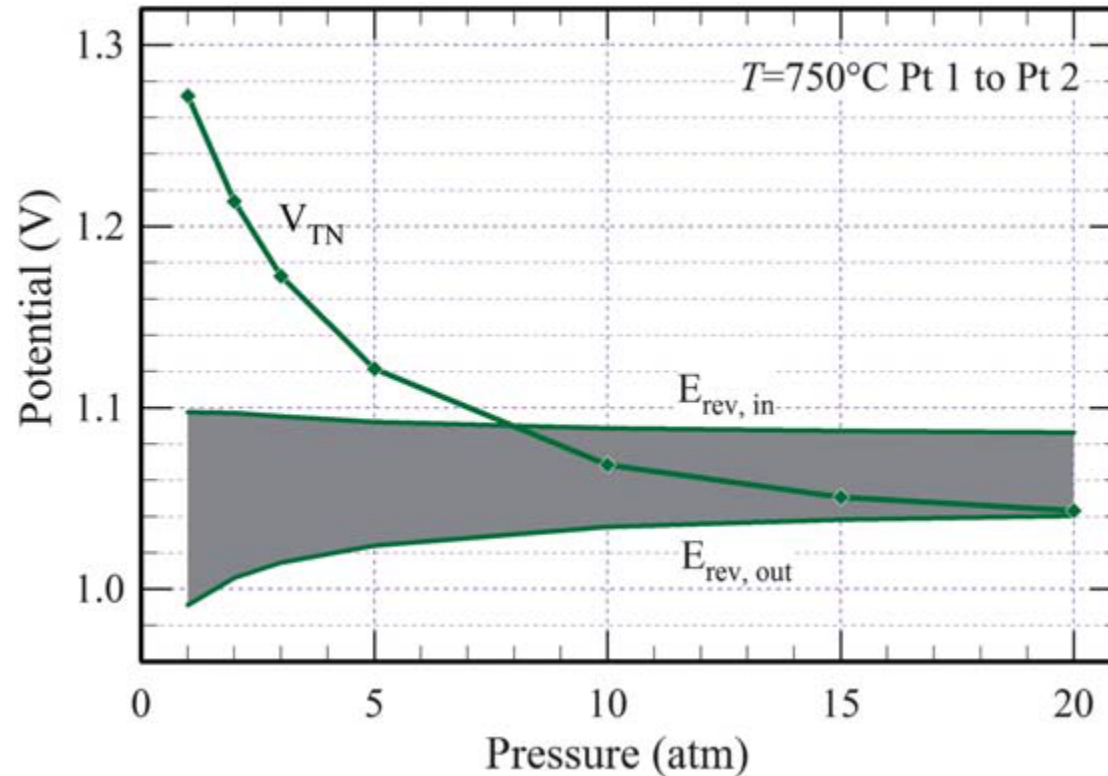
S. H. Jensen, C. Graves, M. Mogensen, C. Wendel, R. Braun, G. Hughes, Z. Gao and S. A. Barnett, *Energy and Environmental Science* **8** (2015) 2471

Pressurized SOCs for large-scale electricity storage



S. H. Jensen, C. Graves, M. Mogensen, C. Wendel, R. Braun, G. Hughes, Z. Gao and S. A. Barnett, *Energy and Environmental Science* **8** (2015) 2471

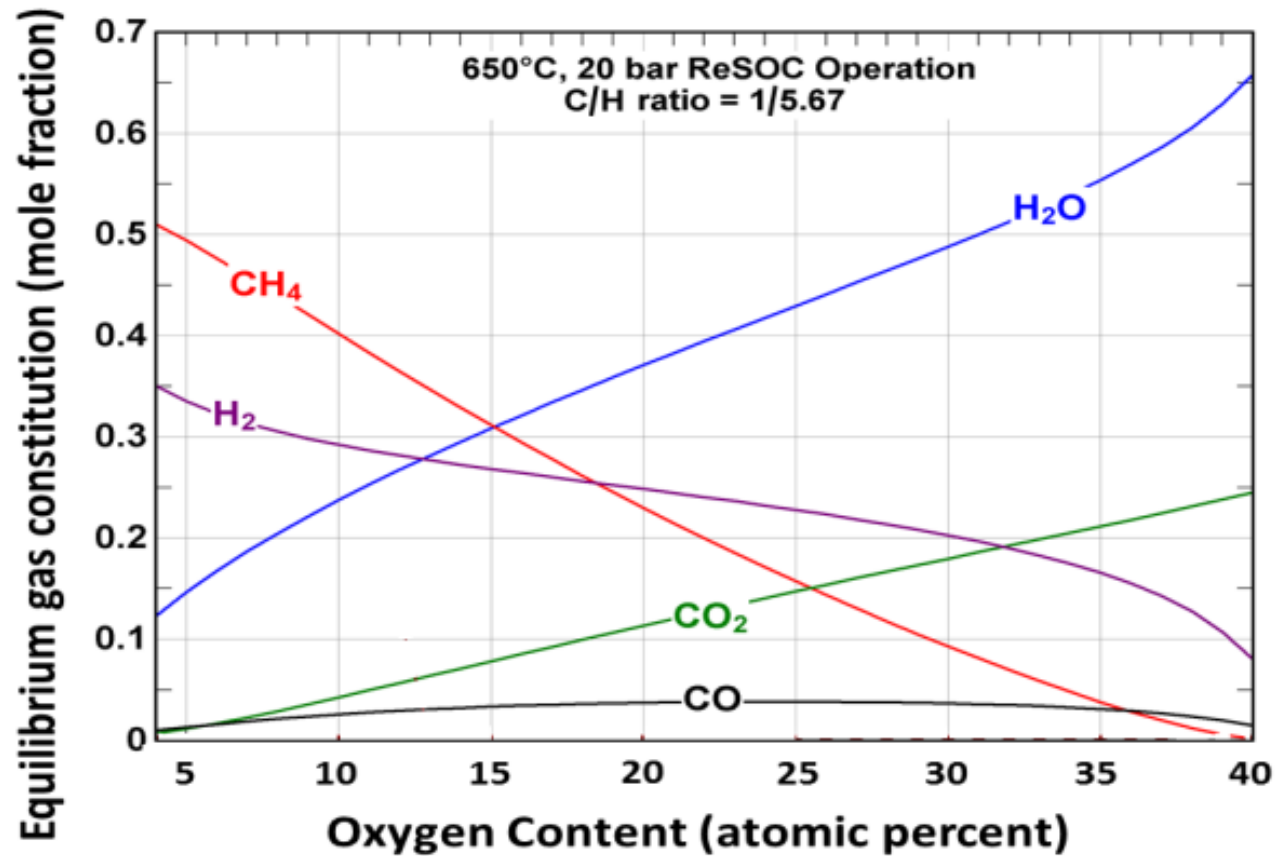
Pressurized SOCs for large-scale electricity storage



Thermal-neutral potentials versus P at $T = 750^\circ\text{C}$ for a cell operating over a fuel composition range from pt 1 to pt 2 (Fig. 3). Shown for comparison are the Nernst potential ranges for fuel compositions from pt 1 to pt 2 and oxygen at the other electrode.

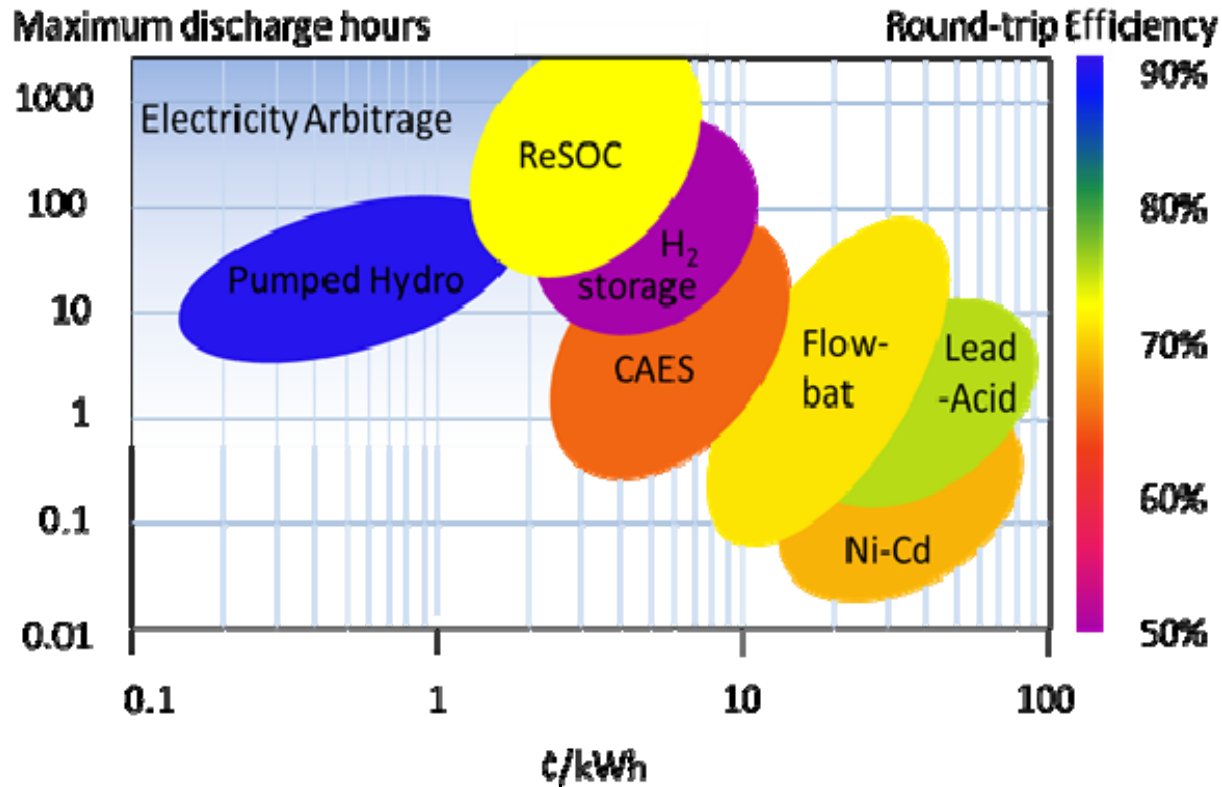
Energy Environ. Sci., 2011, 4, 944–951

Pressurized SOCs for large-scale electricity storage



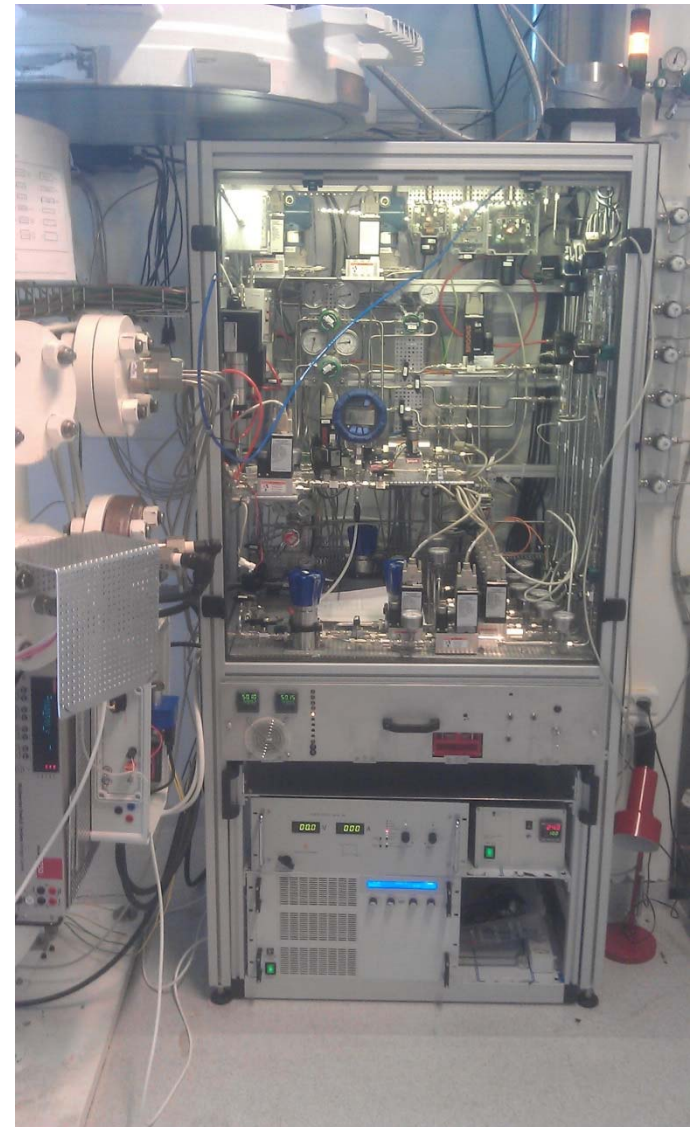
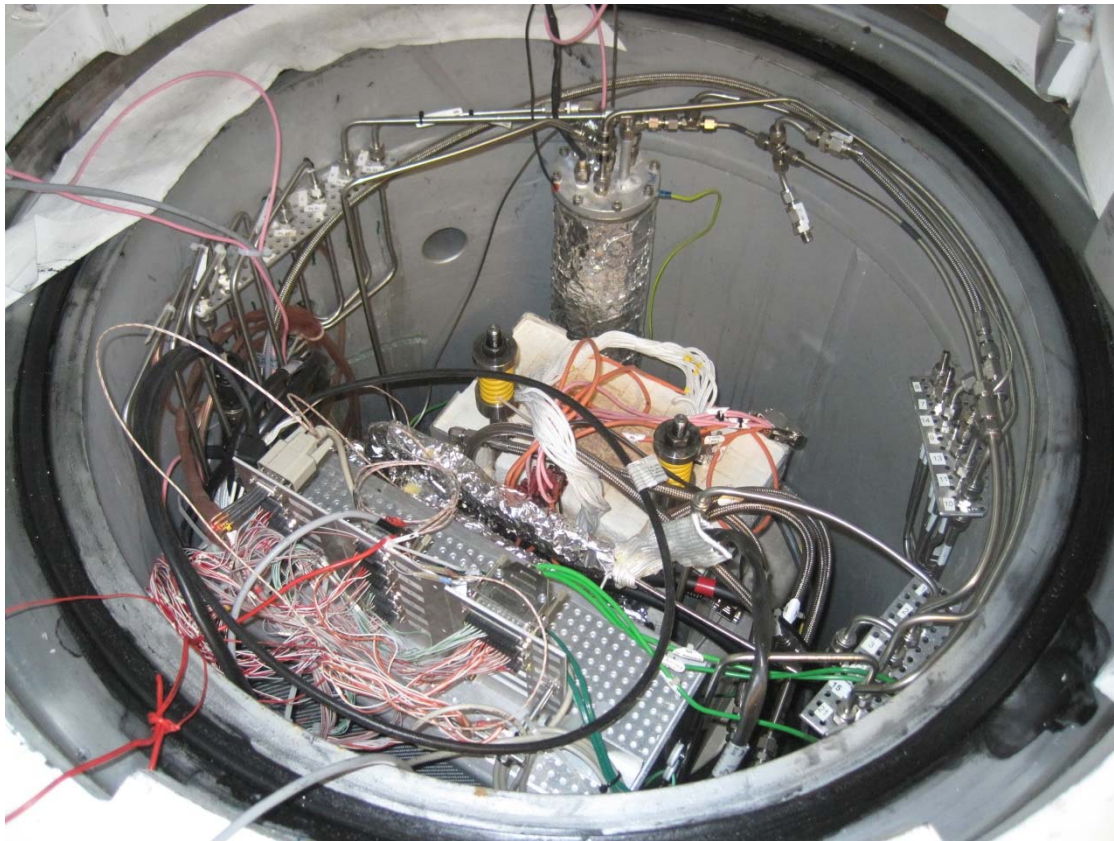
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Pressurized SOCs for large-scale electricity storage

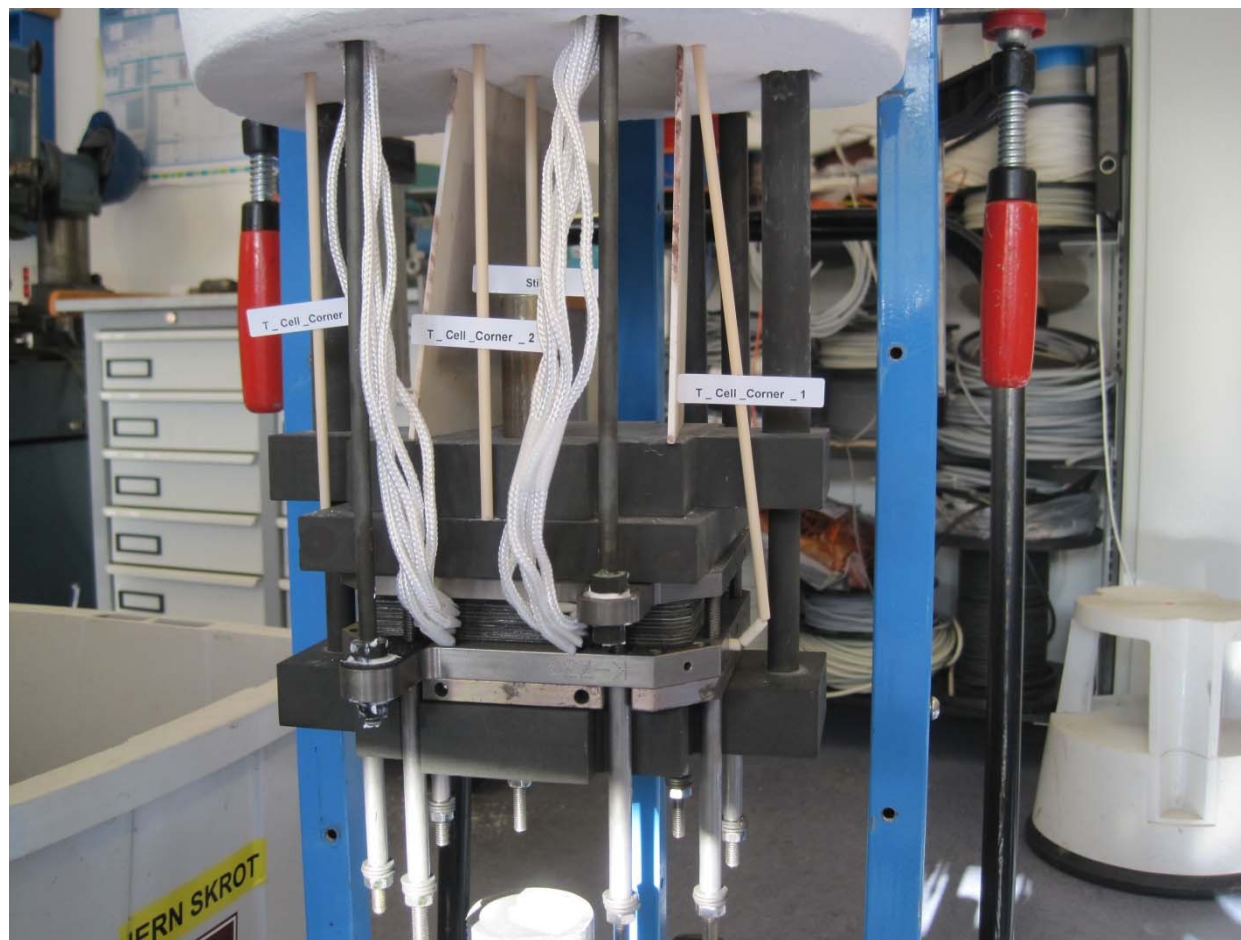


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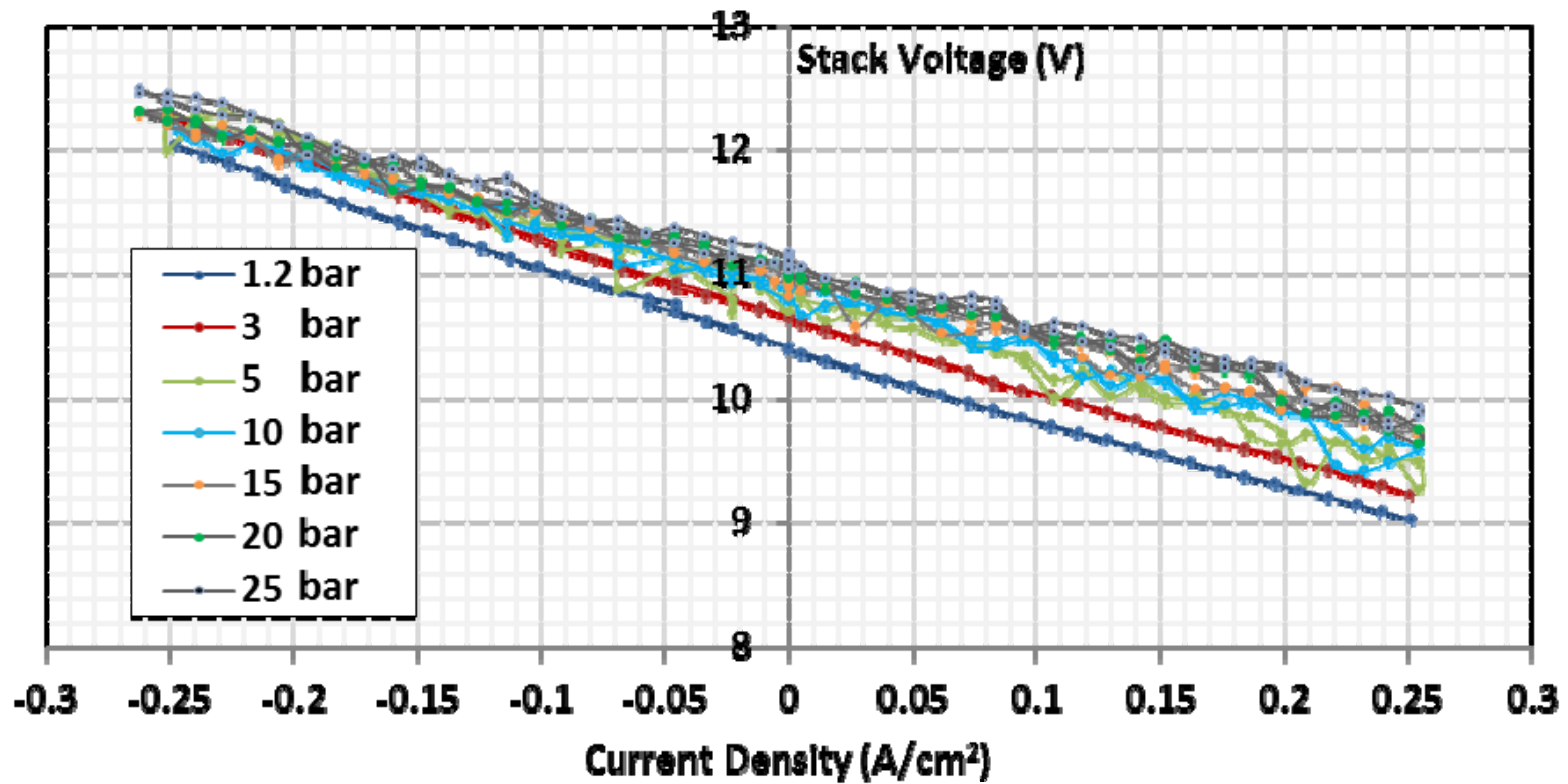
Pressure Test Setup



1 kW SOEC Stack from HTAS



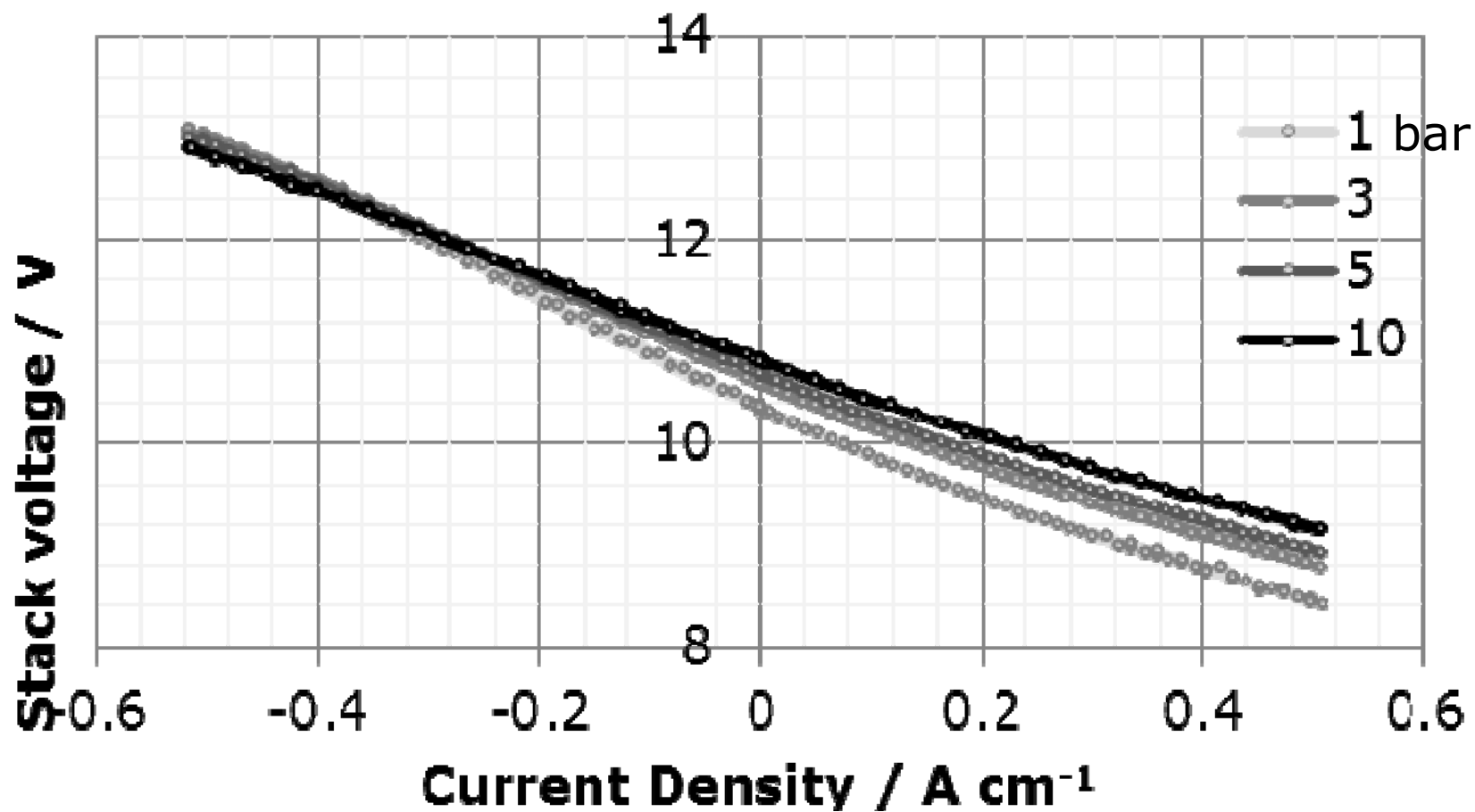
iV curves vs Pressure



S. H. Jensen, X. Sun, S. D. Ebbesen, M, Chen,
Fuel Cells **16** (2) 2016 205-218,
 DOI: 10.1002/fuce.201500180

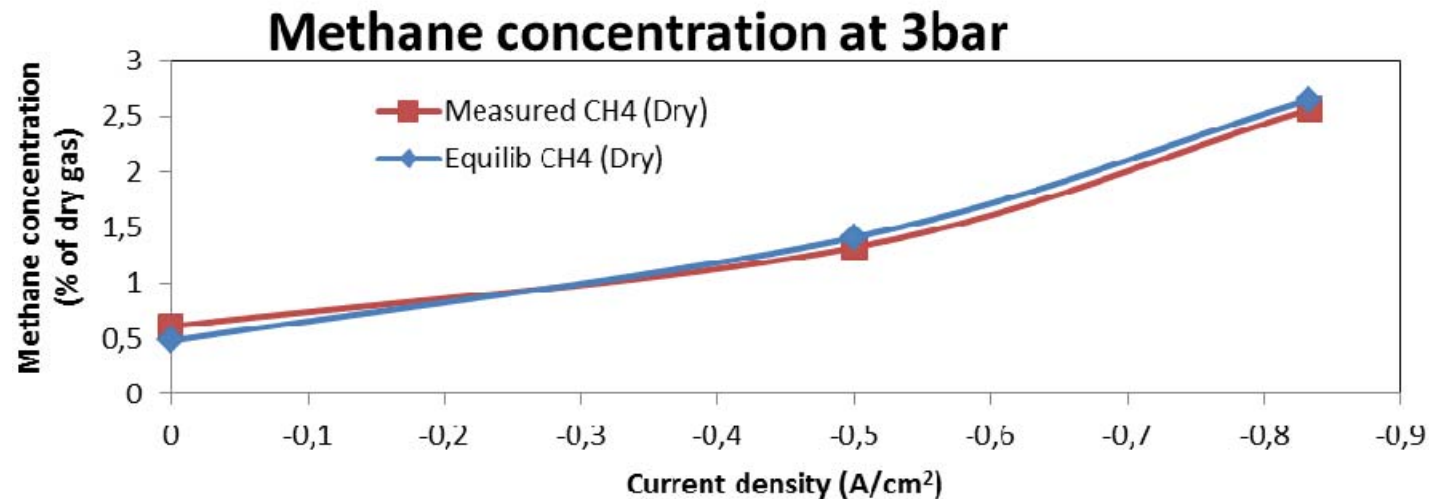
iV curves vs Pressure

50% H₂O + 50% H₂, Air, 750 ° C



S. H. Jensen, M, Chen, X. Sun, C. Graves, J. B. Hansen *To be published in J. Electrochem. Soc*

Internal Methane production in a Planar SOEC



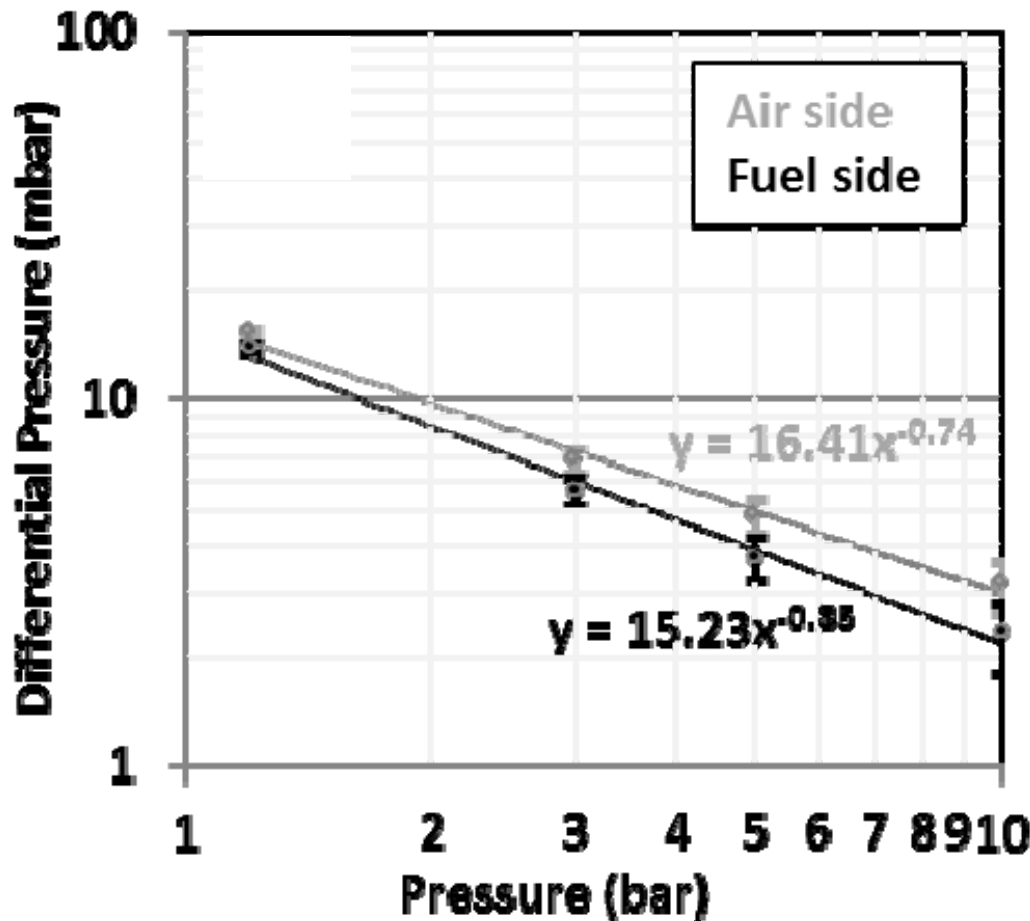
SOEC operating conditions:

- 750°C
- 20 L/h of 50% H₂ + 25% H₂O+25% CO₂ to the fuel electrode
- 50 L/h air to the oxygen electrode

S. H. Jensen, *et al. unpublished work*

Gas Pressure Drop Across the Stack

Operating conditions: 400 l/h Air. 200 l/h H₂ + 200 l/h H₂O. 750 ° c



ΔP across stack and heat exchangers as a function of the gas pressure

Assuming an **isentropic expansion** of the gas through the stack, the **theoretical exponent** for ΔP is **-0.71** for air **-0.75** for 50% H₂ + 50% H₂O

S. H. Jensen, X. Sun, S. D. Ebbesen, M, Chen,
Fuel Cells **16** (2) 2016 205-218,
 DOI: 10.1002/fuce.201500180

Conclusions

Pressurized operation of Planar SOC stacks demonstrates that:

- Gas pressure drop across the stack decreases with pressure \sim (adiabatic) $P^{-0.8}$
- Stable SOEC/SOFC operation with small steam/stack-voltage fluctuations demonstrated at elevated pressure
- ASR decreases with pressure (electrode resistance $\sim P^{-0.3}$)
- Long-term operation at high pressure does not show increase in the degradation rate, although the short test period for the stack test makes this statement a bit uncertain
- Internal Methane Formation is the new black ;-)

Acknowledgement

Thank You For Your Attention

Sponsor Organizations



Projects and Centres

SERC, 2104-06-0011



Solid Oxide Electrolysis for Grid Balancing, 2013-1-12013
and "SOFC4RET", 2014-1-12231

CO₂ Electrofuel, 40000



Green Natural Gas, 64011-0036

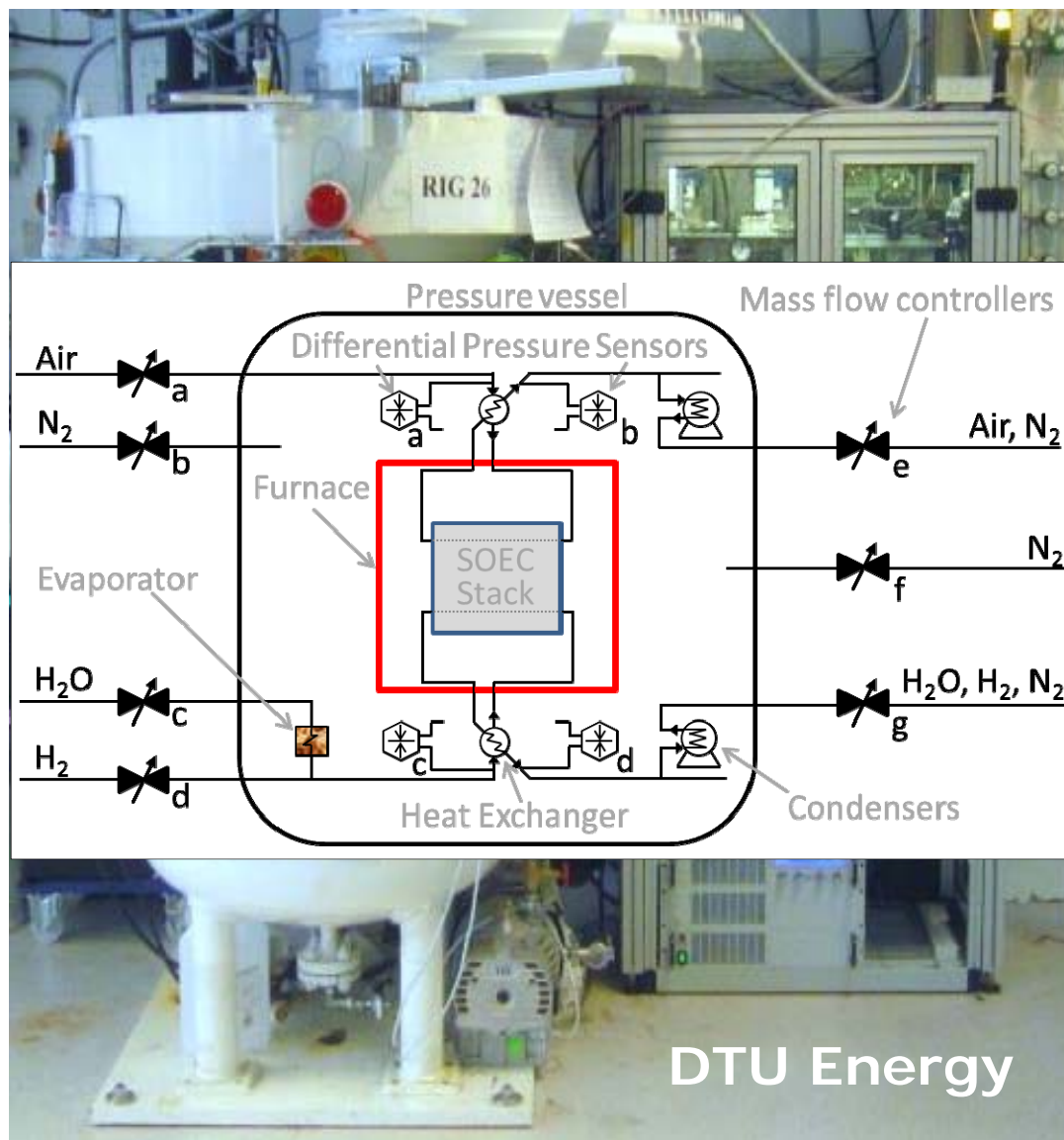
Energi Effektiv Produktion af Tryksat Brint, 64013-0583

SOEC Stack



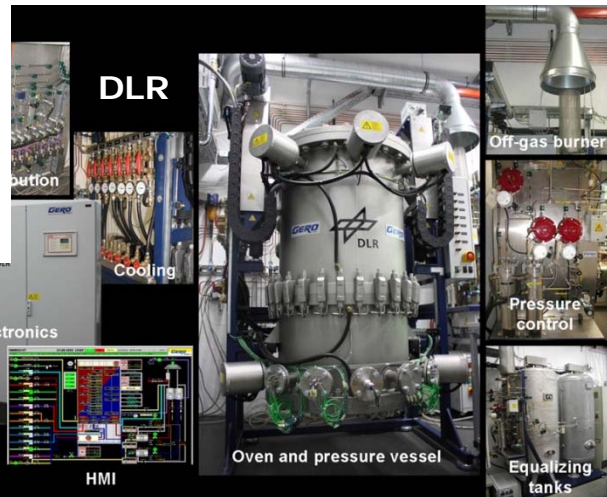
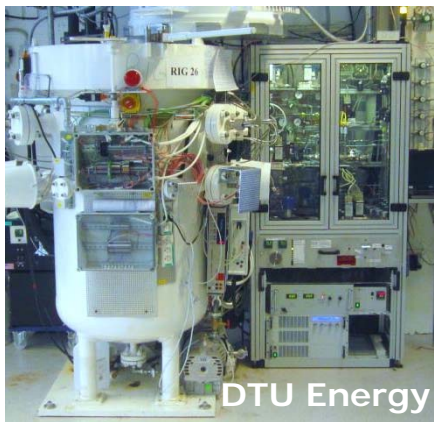
Extra Slides

Pressure Test Setup

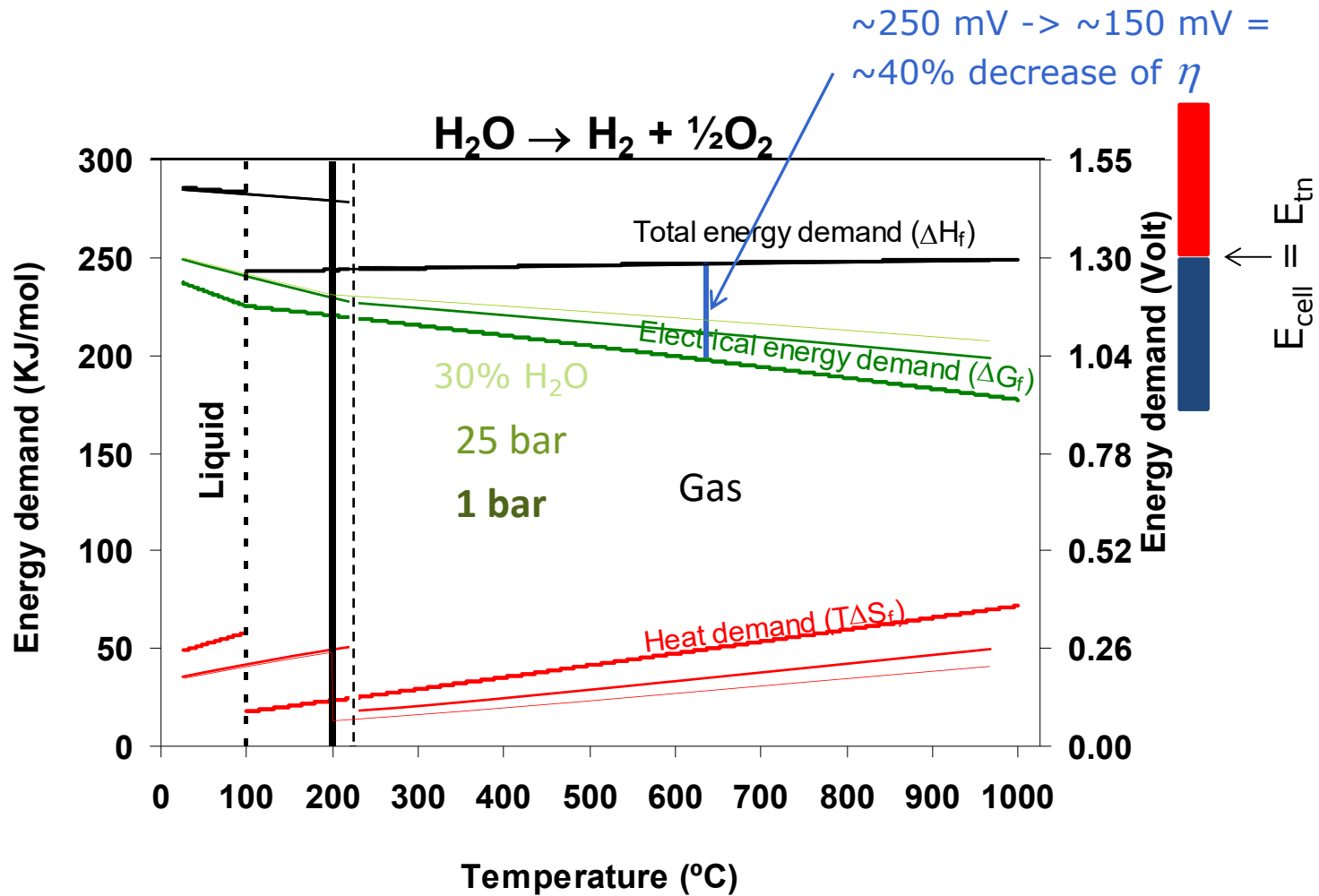


DTU Energy

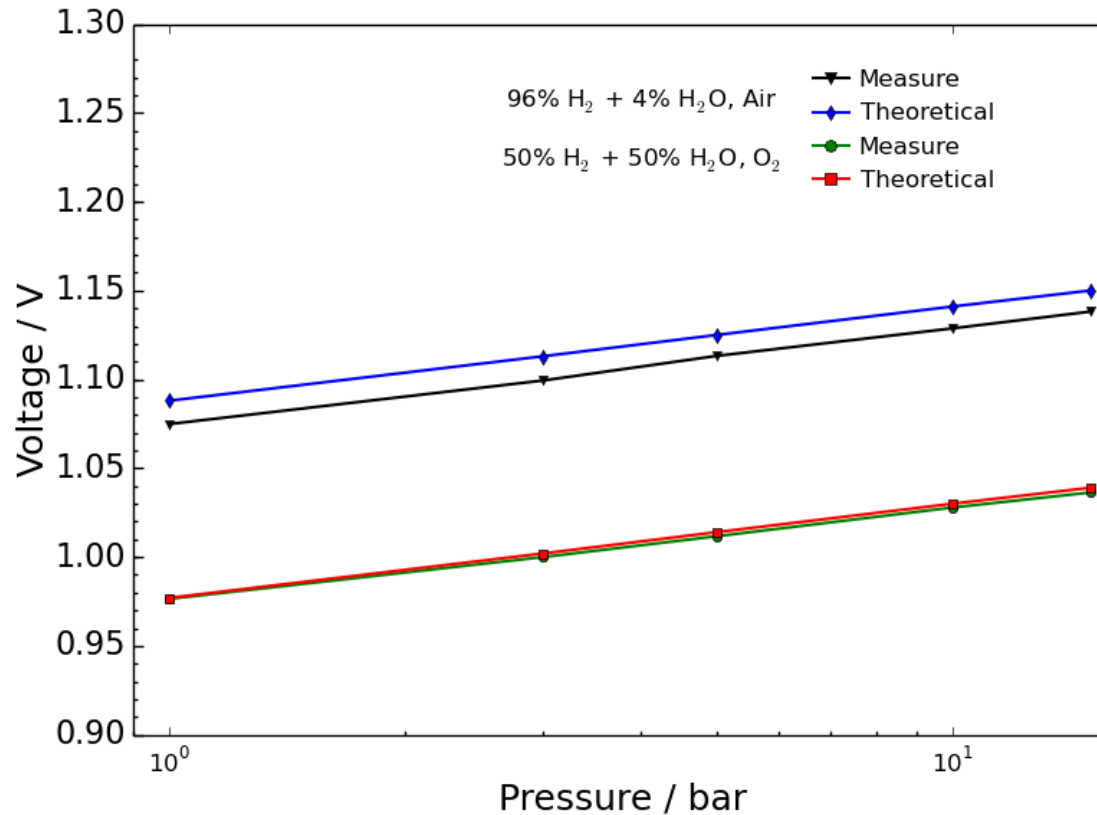
Pressurized SOC activities around the world



Steam Electrolysis Thermodynamics



Steam Electrolysis at Elevated Pressure



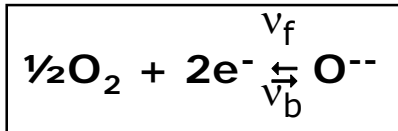
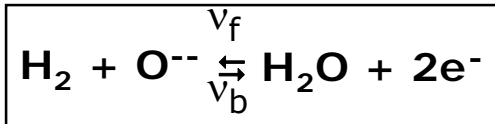
The cell voltage is given by the Nernst equation...

$$E = E_0 + \frac{RT}{2F} \ln \left(\frac{P_{\text{H}_2} P_{\text{O}_2}^{1/2}}{P_{\text{H}_2\text{O}}} \right)$$

...the cell voltage increases with linearly with \ln gas pressure

X. Sun *et al.* submitted to *Fuel Cells*

Electrode Reaction Kinetic

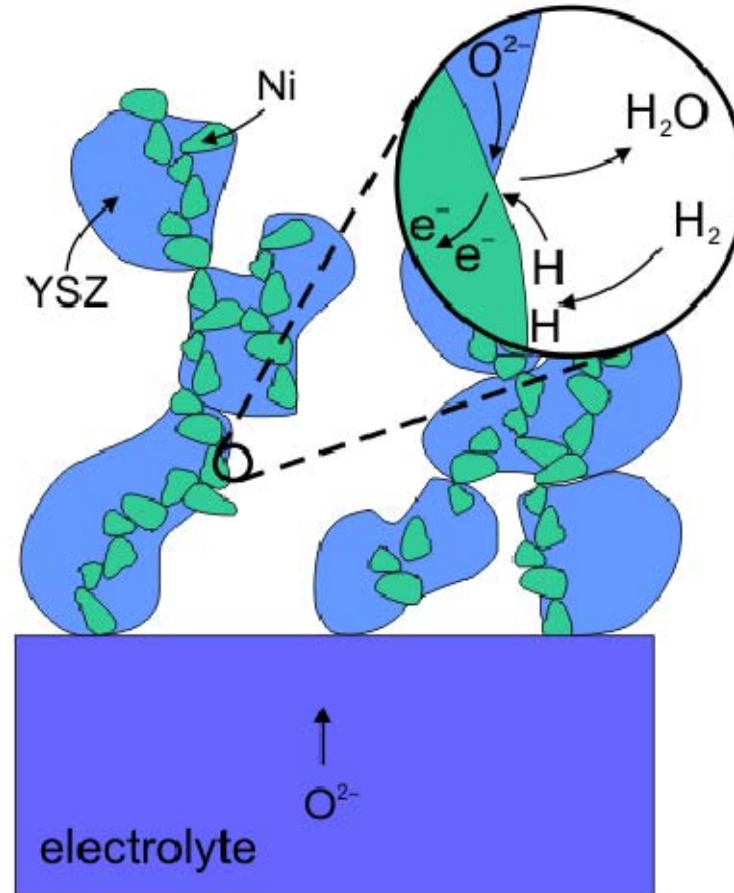


Exchange rates increases with pressure



Gas-solid reaction resistance decreases with pressure

$$R = k(P)^{-n}$$



Pressure and Performance

- J. Høgh have reported $n \sim 0.27$ ($P_{\text{H}_2\text{O}}$ dependence) for DTU Energy Ni/YSZ electrodes*
- Thomsen *et al.* have reported $n \sim 0.25$ for composite LSM/YSZ electrodes**

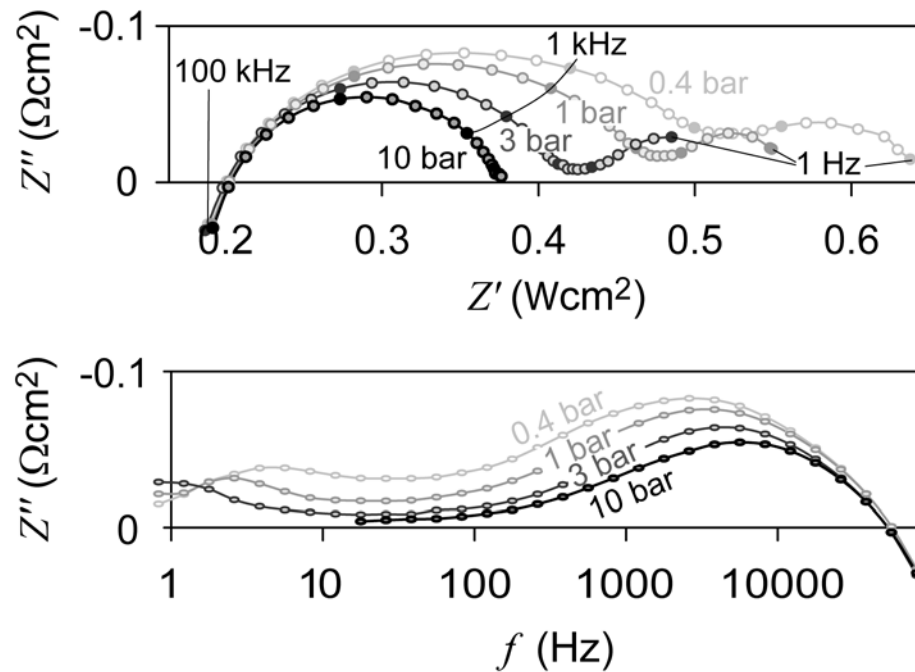
* J. Høgh, *Influence of impurities on the H₂/H₂O/Ni/YSZ electrode*, Risø National Laboratory, Roskilde, Denmark (2005)

** E.C. Thomsen *et al.* *J. Power Sources* **191** (2009) 217–224

$$R = k(P)^{-n}$$

Pressure and Performance

- 750 °C
- Negative Electrode: 20% H₂O + 80% H₂
- Positive Electrode: O₂



Jensen, Sun, Ebbesen, Knibbe, Mogensen. *Int. J. Hydrogen Energy* **35** (2010) 9544

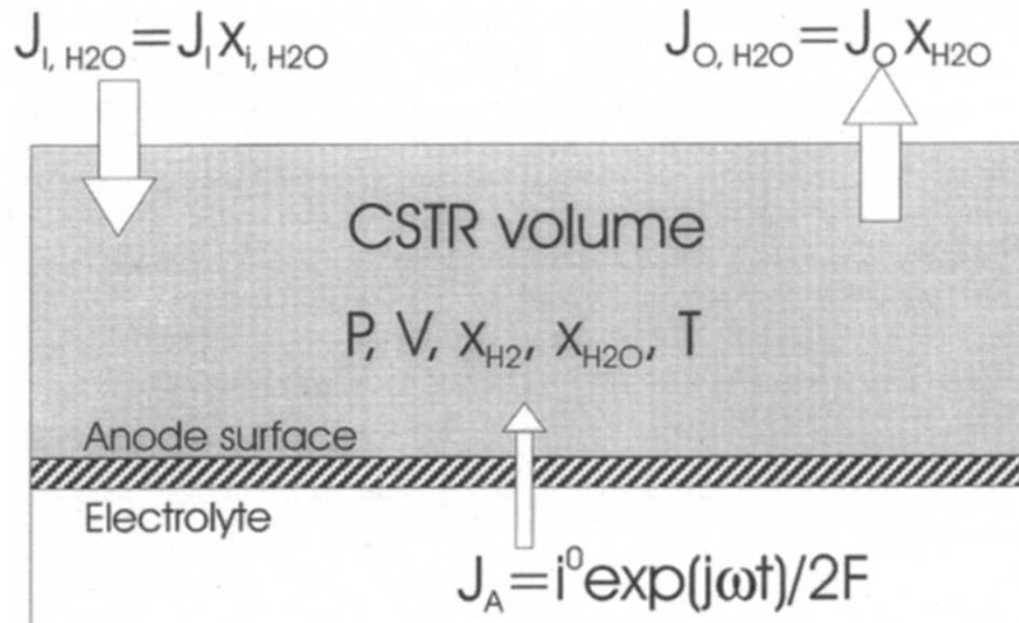
Gas Conversion Impedance

Primdahl and Mogensen. *J. Electrochem. Soc* **145**, 2431 (1998)

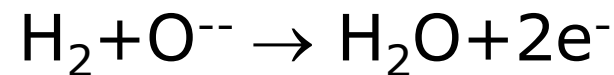
$$R_g = \frac{RT}{4F^2 J_i} \left(\frac{1}{x_{i,H_2O}} + \frac{1}{x_{i,H_2}} \right)$$

$$C_g = \frac{4F^2 PV}{(RT)^2 A} \frac{1}{\frac{1}{x_{i,H_2O}} + \frac{1}{x_{i,H_2}}}$$

$$f_g = \frac{J_i ART}{2\pi PV}$$

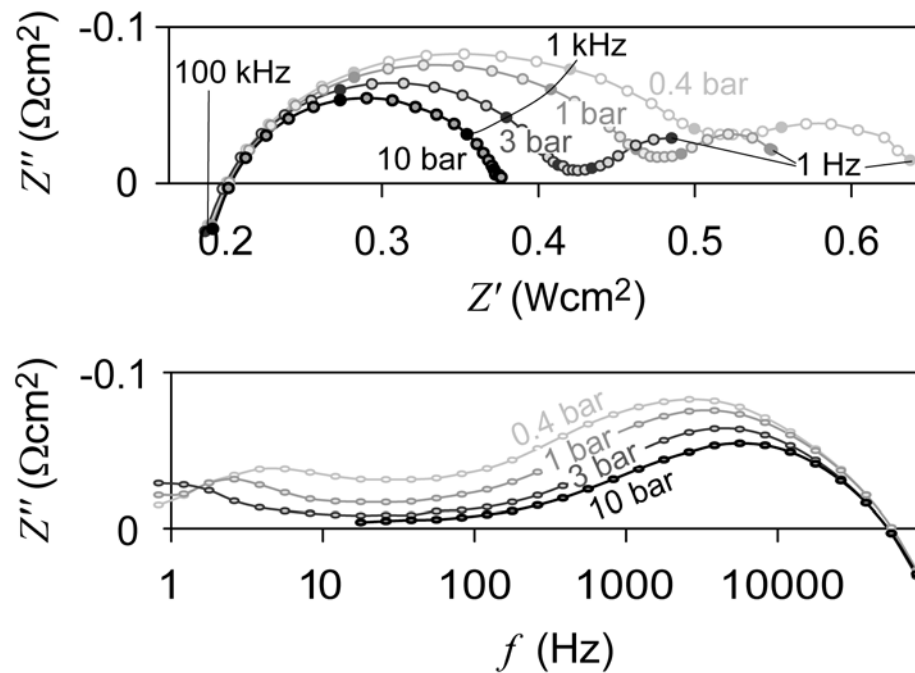


$$J_I = J_O + J_A$$



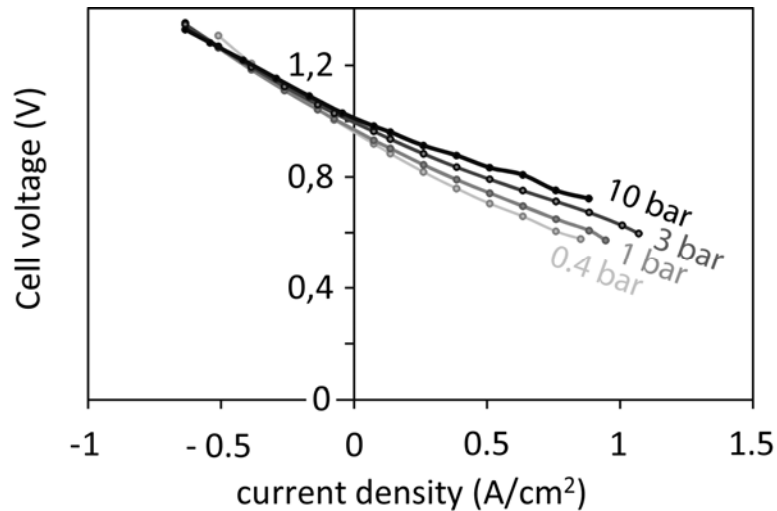
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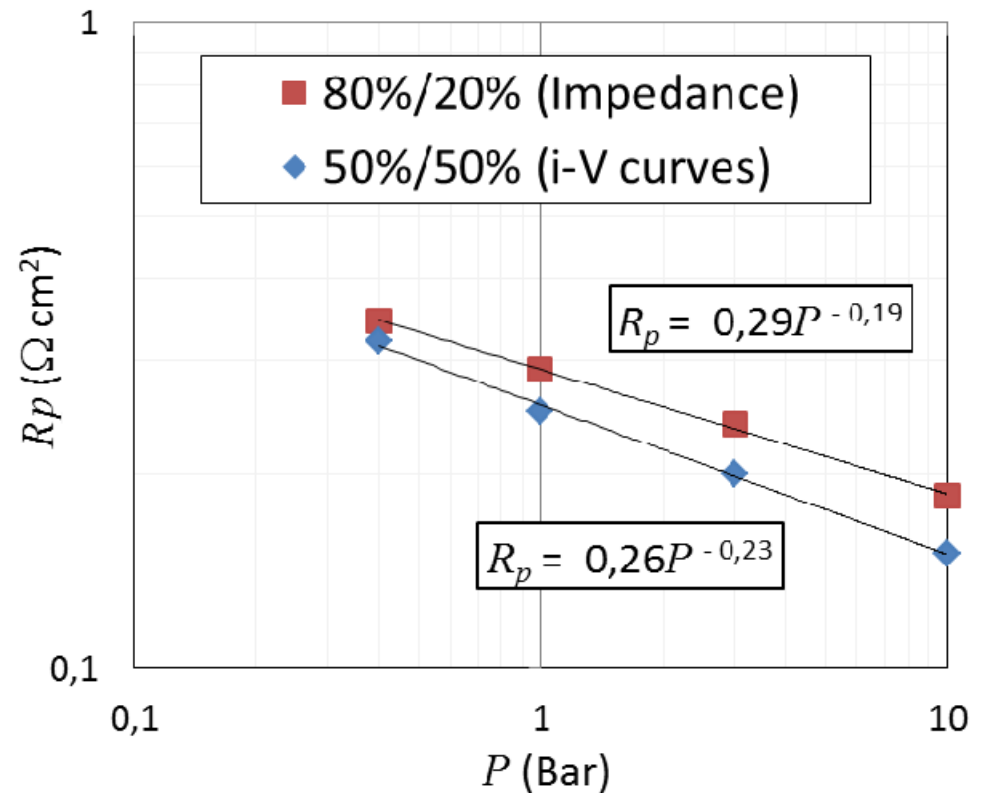
Jensen, Sun, Ebbesen, Knibbe, Mogensen. *Int. J. Hydrogen Energy* **35** (2010) 9544

Pressure and Performance



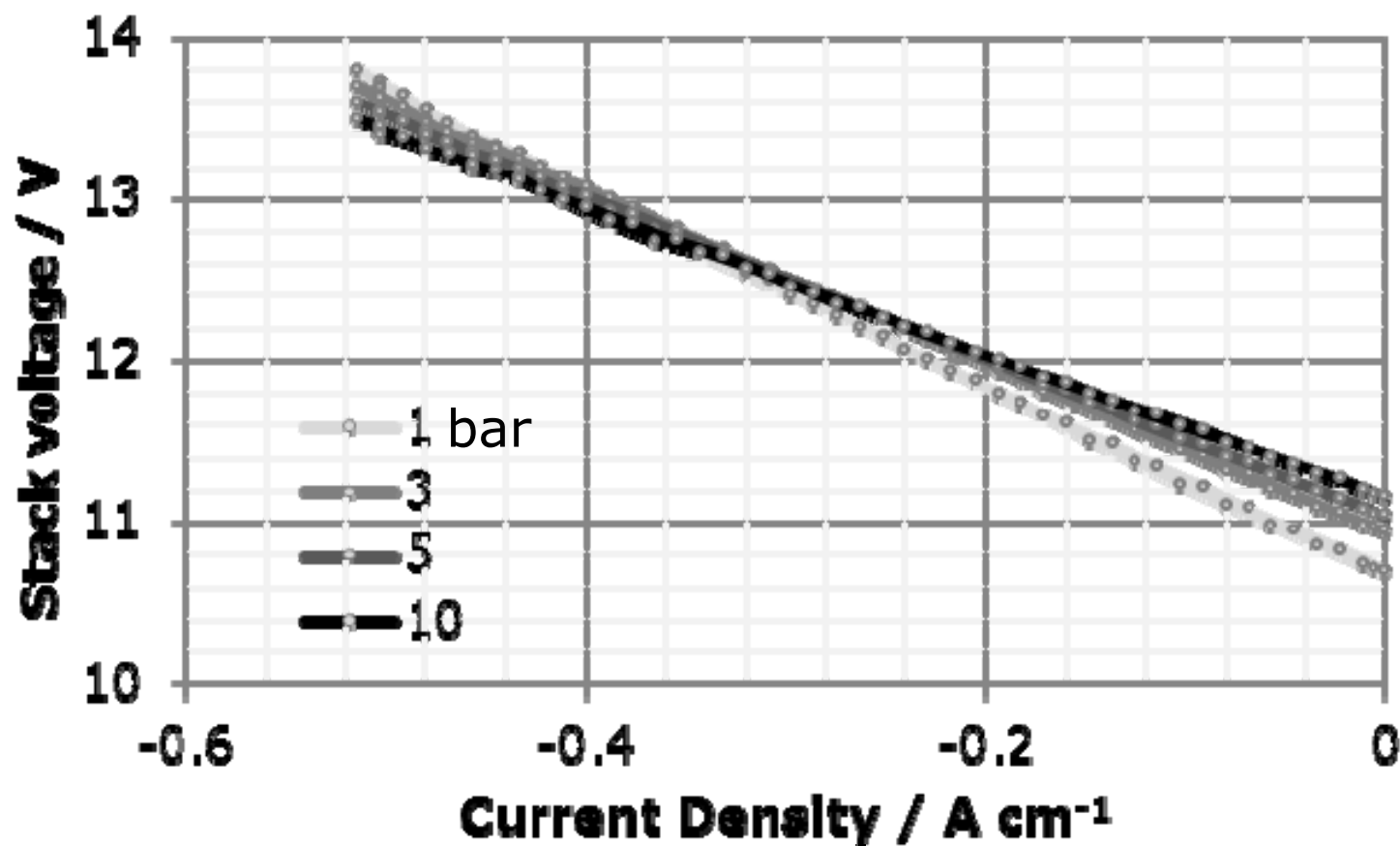
Jensen, Sun, Ebbesen, Knibbe, Mogensen.
Int. J. Hydrogen Energy **35** (2010) 9544

Assuming 70 mΩcm²
gas conversion



“Charge transfer limited reactions involving dissociatively adsorbed oxygen at low Coverage” *E.C. Thomsen et al. J. Power Sources* **191** (2009) 217–224

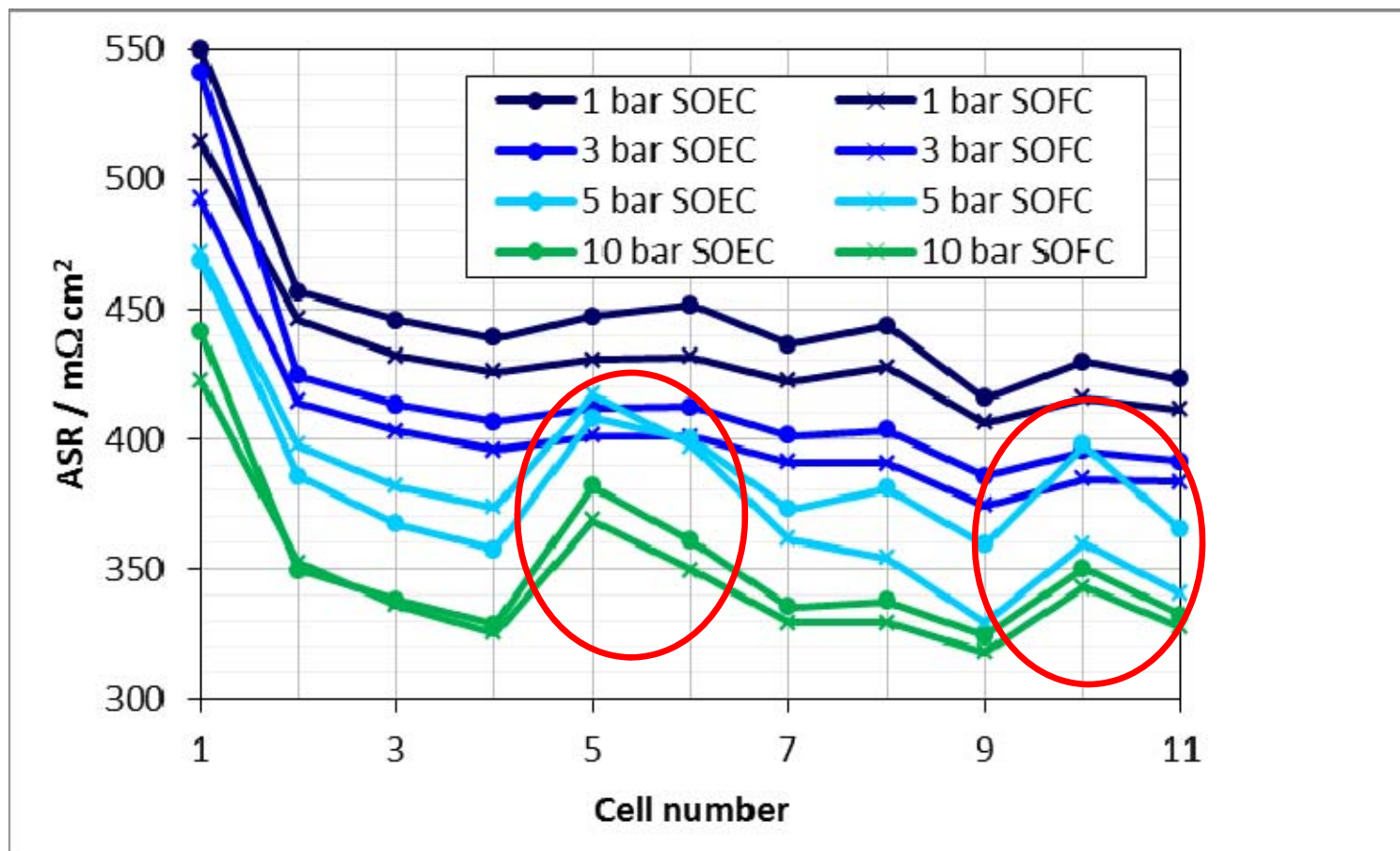
iV curves vs Pressure

33% H₂O + 67% H₂, Air, 750 ° C

S. H. Jensen, M, Chen, X. Sun, C. Graves, J. B. Hansen *To be published in J. Electrochem. Soc*

ASR vs pressure

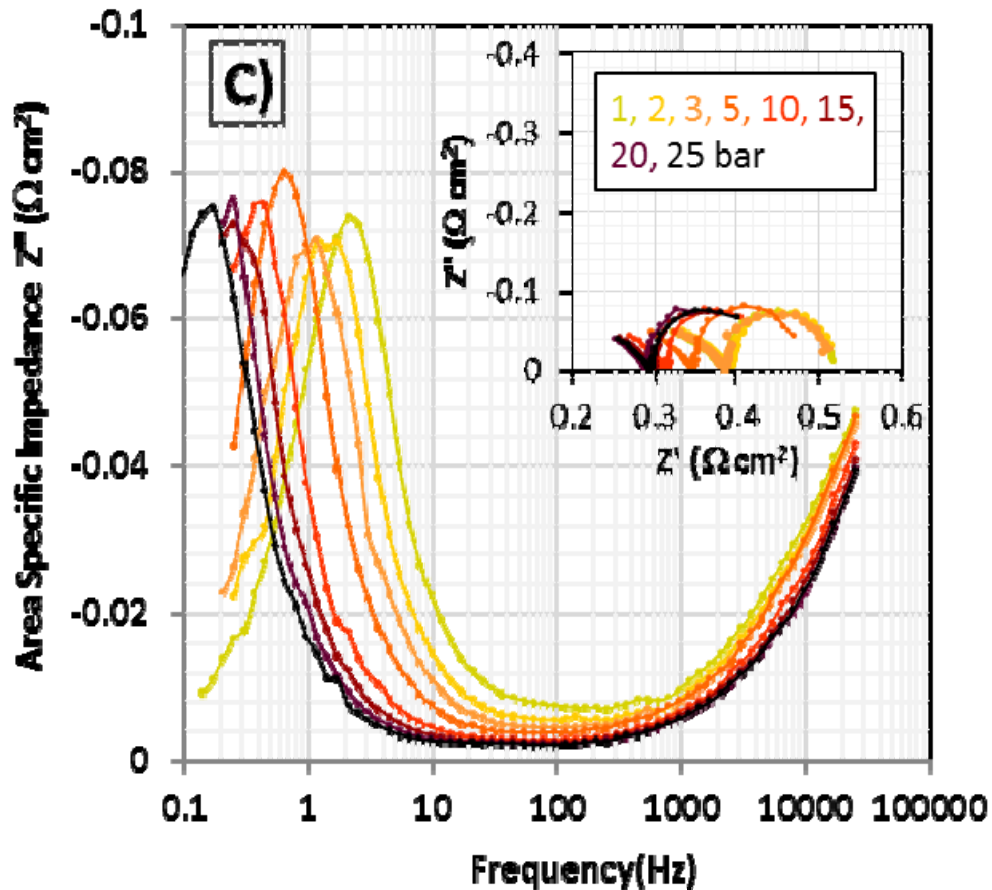
50% H₂O + 50% H₂, Air, 750 ° C



Air starvation during IV curve recorded between 3 and 5 bar

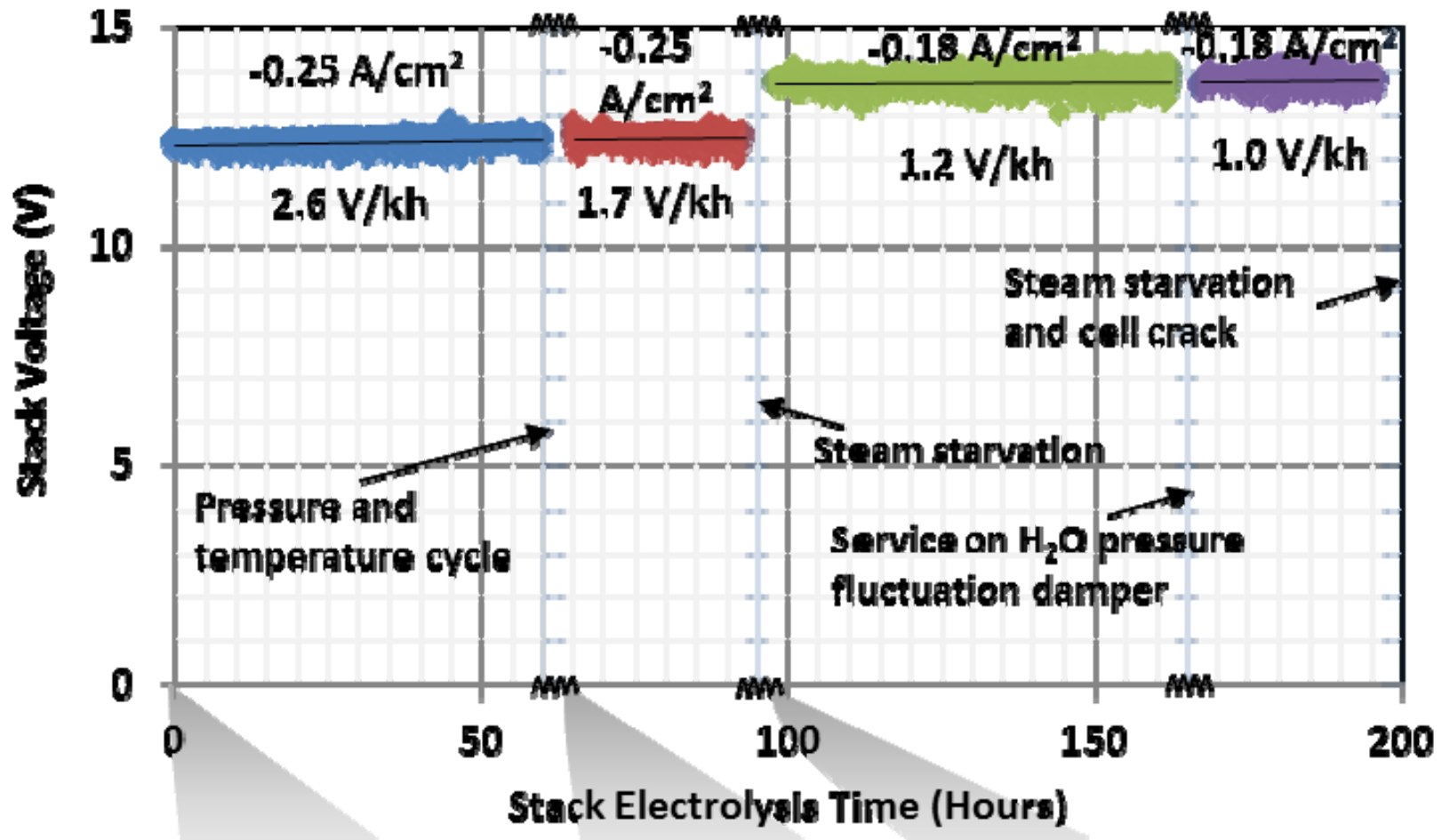
S. H. Jensen, M, Chen, X. Sun, C. Graves, J. B. Hansen *To be published in J. Electrochem. Soc*

Stack Impedance vs Pressure



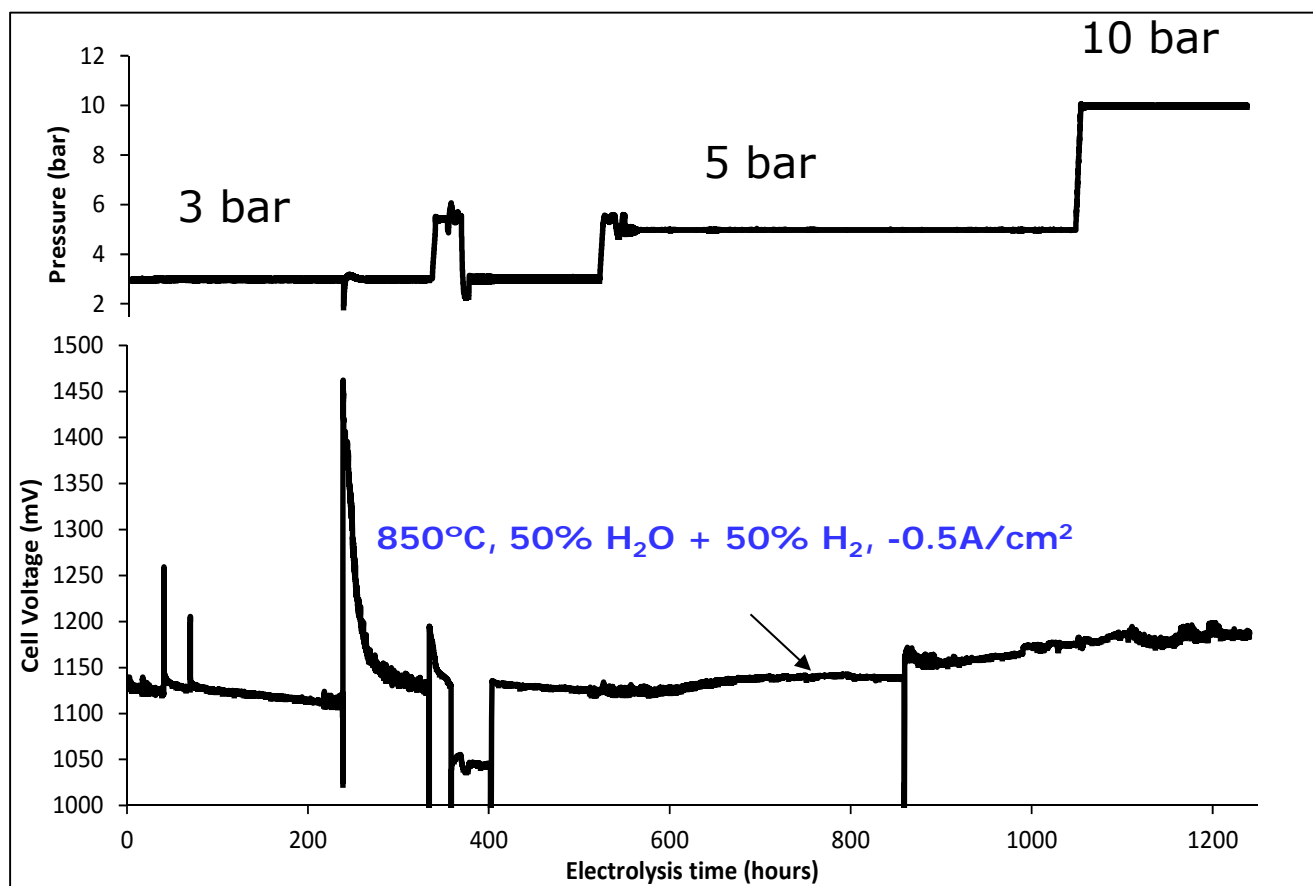
- Low frequency summit frequency decreases with pressure
- The size of the high-frequency arc decreases with pressure

Durability Test at 10 bar



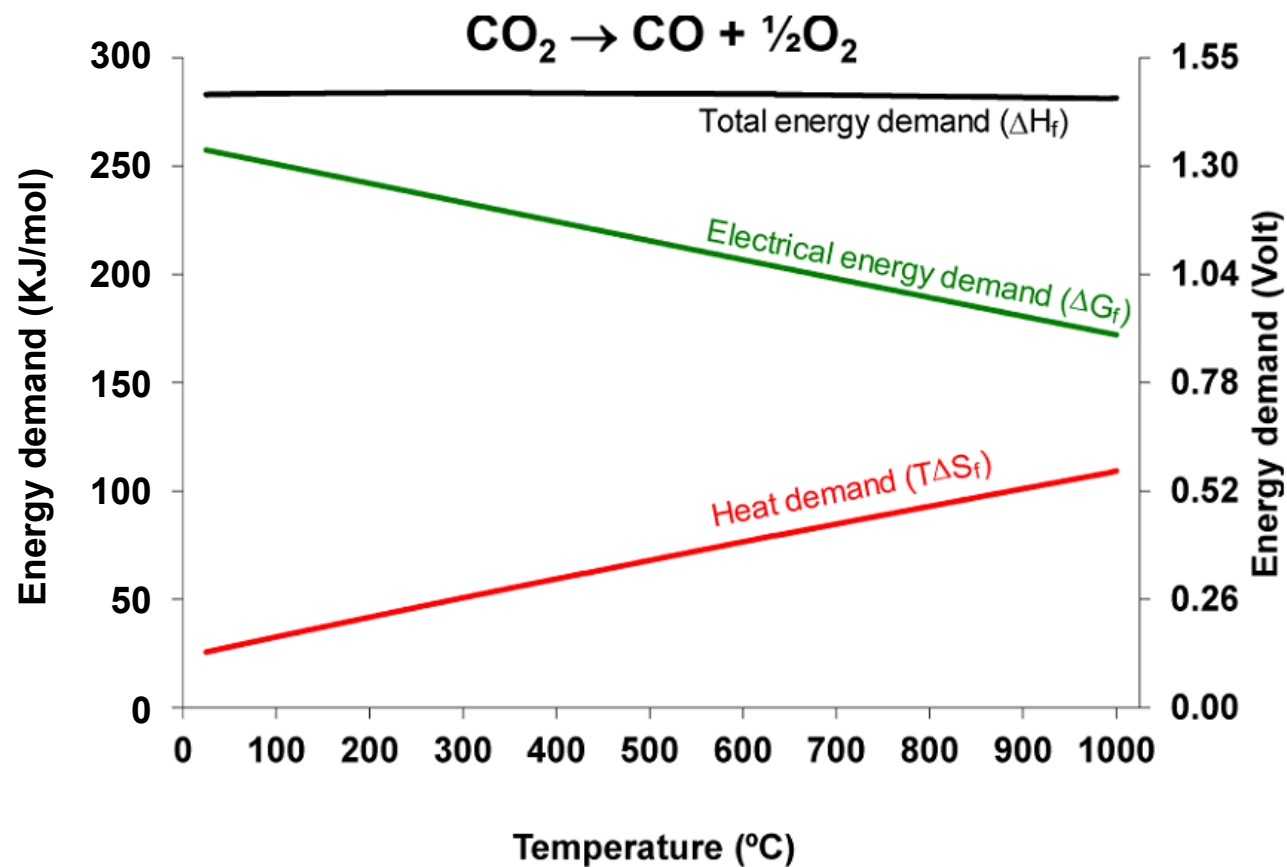
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Durability Test



S. H. Jensen, *et al.* unpublished work

CO₂ Electrolysis Thermodynamics



CH₄ Formation Thermodynamics

